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Indirect evaporative combined inlet air cooling with gas turbines for green power technology



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ABSTRACT

Different inlet air cooling systems are usually used with gas turbines. A new form of inlet air cooling called the indirect evaporative cooling system (IECS) has been investigated in this work. This system is a combination of a humidifier with a vapor compression or absorption cooling system for part of the total air i.e. the secondary air stream. The net power produced from the gas turbine on a hot day (45 °C) by using combined (IECS) with absorption chillers showed an increase in power and efficiency by 15% and 9%, respectively; its recovery period is suitable for all environmental conditions. For IECS combined with vapor compression mechanical chillers showed an increase in power and efficiency by about 7.81% and 2.24%, respectively, but its recovery period made it suitable only for hot and humid conditions. The IECS has lower chiller's capital cost by about 25% (mechanical chiller) and 40% (absorption chiller).

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Refroidissement évaporatif de l'air entrant combiné à des turbines à gaz pour une technologie de production d'électricité écologique

Mots clés : Systèmes de refroidissement de l'air entrant ; Turbines à gaz ; Refroidissement évaporatif indirect (IECS) ; IECS avec refroidisseur à absorption ; IECS avec refroidisseurs mécaniques ; Technologie écologique

1. Introduction

Gas turbines are engines often used to produce electricity. Their capacity and efficiency are lowered as the ambient temperature

is increased. At a given shaft speed, they always move the same volume of air, but the power output of such engines depends on the mass flow passing through it. This is precisely the reason why on hot days, when the air is less dense, power output falls off. Many techniques, including evaporation, fogging, vapor

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Nomenclature
                                                                             effectiveness
                                                                    3
                                                                    Φ
                                                                             relative humidity
                                                                    ??
                                                                             specific heat ratio
Symbols
                                                                    ω
                                                                             humidity ratio [kg<sub>w</sub> kg<sub>a</sub><sup>-3</sup>]
Α
         area [m2]
         ratio of the cooled air mass flow to the
A_r
                                                                    Suffixes
         total air mass flow rates
                                                                             air
         specific heat at constant pressure [kJ (kg K)-1]
Ср
                                                                    abs.A
                                                                             absorber
COP
         coefficient of performance
                                                                    amb
                                                                             ambient temperature
f
         fuel air ratio
                                                                    cond,C
                                                                             condenser
h
         specific enthalpy [kJ kg-1]
                                                                    comp,c compressor
IECS
         indirect evaporative cooling system
                                                                    db
                                                                              dry bulb temperature
m
         mass flow rate [kg s-1]
                                                                             evaporator
                                                                    evap,E
\dot{M}_{weak}
         mass flow rate of weak solution of Li-Br [kg s-1]
                                                                             gas
                                                                     g
P_c
         power consumed by compressor [kW]
                                                                    gen,G
                                                                             generator
         net power output from gas turbine [kW]
P_{\text{G.T}} \\
                                                                    GT
                                                                              gas turbine
Q°
         heat transfer rate [kW]
                                                                    hex
                                                                             heat exchanger
SFC
         specific fuel consumption [kgf kWh<sup>-1</sup>]
                                                                    Li—Br
                                                                             lithium bromide
Т
         temperature [°C]
                                                                             refrigerant
                                                                    ref
TIT
         turbine inlet temperature [°C]
                                                                             saturated
                                                                    sat
         specific volume [m³ kg-1]
v
                                                                             theoretical analysis
                                                                    th
         concentration of Li-Br [kg LiBr kg-1 mix]
х
                                                                             vapor compression
                                                                     υc
rc
         pressure ratio
                                                                              water
                                                                    w
                                                                             inlet water
                                                                    wi
Greek letters
         efficiency %
η
         density [kg m<sup>-3</sup>]
ρ
```

compression, thermal storage and absorption, have been developed to cool the inlet air to the gas turbine engine (Al-Ibrahim and Varnham, 2010; Alhazmy and Najjar, 2004; Bacigalupo et al., 1993; Bedecarrats and Strub, 2009; Korakianitis and Wilson, 1994; Lucia et al., 1994, 1996; Lukas, 1997; Najjar, 1996; Yokoyama and Ito, 2004). Moreover, unconventional techniques have been suggested (Anonymous, 2002a; El-Hadik, 1990; Khaliq et al., 2010; Liu et al., 2009; Zamzam and Al-Amiri, 2008).

Traditionally, the inlet air is cooled by either direct evaporative system or indirect evaporative system. Evaporative cooling is a simple and effective way of cooling the air stream in a direct evaporative cooler. The air stream to be cooled is directly in contact with a liquid water film and the cooling is accomplished by the adiabatic heat exchange between the air stream and the liquid water film (Jolly, 2000). The evaporation of water in the air stream leads to a reduction in the dry bulb temperature. However, this will also cause an increase of the humidity ratio of the air stream. Johnson (1989) establishes the basic theory, whereas applications are handled in details in the reference (Agren and Westermark, 2003a, 2003b; Anomymous, 2001; Biasi, 2000a; Farmer, 1999, 2009; Robb, 2001).

Another approach for cooling the inlet air to the gas turbine is by introducing liquid water into the suction air. The water droplets will have to be extremely small in size and be in the form of fog to avoid impingement on the blades of the compressor causing erosion (Lukas, 1997).

As the water evaporates within the compressor from the heat of compression, the air being compressed is cooled, which

in turn causes a reduction in the compressor work (Anonymous, 2001, 2002b; Biasi, 2000b; Bird and Grabe, 1991; Bucker et al., 003; Chacker et al., 2004a, 2004b; Chaker et al., 2004; Farmer, 2008; Homji and Mee, 1999; Levy et al., 2008; Mee, 1999).

The ideal vapor-compression cycle uses refrigerant as the working fluid to absorb and reject heat energy. The energy transfer allows the vapor-compression cycle to cool the inlet air to the gas turbine (Cengel and Boles, 2010).

Absorption chillers differ from the more prevalent compression chillers in that the cooling effect is driven by heat energy, rather than mechanical energy. Additionally, absorption systems use distilled water and either nontoxic lithium bromide or ammonia, thereby eliminating harmful chlorofluorocarbons (CFCs) common to a vapor-compression systems (Alhazmy and Najjar, 2004; Najjar, 1996). More details of the absorption system with gas turbines are in the reference (Baughn and Kerwin, 1987; Blanco, 1993; Bruno et al., 2005; Hong et al., 2010; Malewski and Holldorff, 1986; Stambler, 1989; Yang and Sato, 1971; Yang et al., 1970, 1971; Yin et al., 2010). Currently, available water-cooled absorption systems use water as the refrigerant and lithium bromide solution as the absorbent material. In the aqua–ammonia systems, ammonia is used as the refrigerant and water as the absorbent.

The indirect evaporative cooling system IECS produces cooling by directly evaporating water into a part of the main air stream (secondary air). This secondary air is then cooled in a refrigeration system before final mixing with primary air (combined system). This supplementary cooling of the air when passing over the evaporator of the refrigeration system will

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