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Exergoeconomic performances of the desiccantevaporative air-conditioning system at different regeneration and reference temperatures



^a Enteria Grün Energietechnik, Davao 8000, Philippines

^b Tohoku University, Sendai 980-8579, Japan

^c Building Research Institute, Tsukuba 305-0802, Japan

^d Architectural Institute of Japan, Tokyo 108-8414, Japan

^e Maeda Corporation, Tokyo 179-8914, Japan

^f Akita Prefectural University, Akita 010-0195, Japan

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ABSTRACT

This paper presented the exergoeconomic evaluation of the developed desiccantevaporative air-conditioning system. The developed system was evaluated based on the steady-state conditions at different regeneration and reference temperatures. The exergoeconomic evaluation method was implemented to the system components and the whole system to evaluate the exergy efficiency, exergy destruction ratios, cost rates, relative cost differences and exergoeconomic factors. The regeneration and reference temperatures affected the exergy efficiencies, exergy destruction ratios, cost rates, relative cost differences and exergoeconomic factors. The desiccant wheel, heating coil and evaporative cooler had a high cost rate (investment cost, operation and maintenance cost, and exergy destruction cost). The exit air fan, outdoor air fan and evaporative cooler had a high relative cost difference. The exit air fan, outdoor air fan and secondary heat exchanger had a high exergoeconomic factor. Replacement of the desiccant wheel with a higher dehumidification performance could decrease the high cost rate. A higher efficiency evaporative cooler and heating coil were needed. Cheaper air fans (outdoor air fans and exit air fans) were needed. © 2014 Elsevier Ltd and IIR. All rights reserved.

Performances exergo-économiques d'un système de conditionnement d'air évaporatif à déshydratant à différentes températures de régénération et de référence

Mots clés : Thermodynamique ; Exergoéconomique ; Deshumidification á deshydratant ; Refroidissement évaporatif

^{*} Corresponding author. Enteria Grün Energietechnik, Davao 8000, Philippines. Tel./fax: +63 (0) 82 305 2226. E-mail address: enterian2@asme.org (N. Enteria).

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Nomenclatures		ω	humidity ratio (g kg $^{-1}$)	
c cost n	per every rate (\$/bw)	φ	annual maintenance factor	
e cost p	$\frac{1}{2} c e^{-1}$	ε	exergy efficiency	
f everge	n economic factor	Supersci	rint	
i intere	interest rate		CL component investment	
<i>m</i> mass	flow rate $(kg s^{-1})$	OM	operating and maintenance	
n total c	pherating period (Year)	0111	operating and maintenance	
r relativ	relative cost difference		Subscript	
t time (1,2	air state point	
Ċ evero	$x \cos t rate ($/h)$	е	exit	
CRF capita	l recovery factor	D	destruction	
D destru	iction	DW	desiccant wheel	
DW desico	ant wheel	EC	evaporative coil	
Ė evero	v rate (kW)	F	fuel	
FC evano	rative coil	F _{OA}	outdoor air fan	
Ec evapo	or air fan	F_{EA}	exit air fan	
F _{EA} exit ai	ir fan	HC	heating coil	
HC heatin	ng coil	HX_1	primary heat exchanger	
HX ₄ prima	ry heat exchanger	HX_2	secondary heat exchanger	
HX _o second	dary heat exchanger	i	inlet	
IC invest	tment cost (\$)	k	kth component	
L loss		L	loss	
MX flow n	nixer	ṁ	mass flow rate	
N annua	al operating hour	Ν	node	
OMC operat	tion and maintenance cost (\$)	Р	product	
0 heat t	ransfer rate (kW)	q	heat	
T tempe	erature (°C)	r	reference conditions	
Ŵ work	rate (kW)	Tot	total	
Ż capita	l cost rate (\$/h)	ω	work	
- aprica	(†)/	W	water	
Greek symbols				

1. Introduction

Maintenance of the indoor environmental conditions is one of the energy intensive parts of a house's or building's operation. In hot and humid climates, air dehumidification and cooling consume a large percentage of buildings' electric energy (Kong et al., 2012). As people stay indoors most of the time, it is expected that the maintenance of the indoor environment will become more intensive as the population explosion, urbanization and industrialization became more prevalent (Enteria, 2013).

The desiccant-based air-conditioning system is one of the most promising alternative systems in the maintenance of indoor temperature and humidity. The desiccant-based system can control air thermal contents (latent and sensible) (Enteria, 2013), micro-organisms (viruses and bacteria) (Goswami et al., 1997) and chemical contents (such as VOCs) (Fang et al., 2008). As the system can be supported by different energy sources, it is flexible depending on the on-site available energy sources (Enteria and Mizutani, 2011). However, since the desiccant-based air-conditioning system consumes energy from different sources (such as electric, thermal and hydro) (Enteria and Mizutani, 2011), exergy analysis is important (Bejan et al., 1996). In addition, as different sources of energy have different costs, the combined exergy and economic analysis is a very important factor for the system evaluation. Hence, application of the exergoeconomic evaluation is an important component for determining the thermal and economic performance of the thermal systems (Bejan et al., 1996; Tsatsaronis, 1996).

Tsatsaronis (1993) presented the review of the exergy analysis and the thermo-economic analysis performance of the energy systems. It shows that thermo-economic analysis is an important tool for the determination of the cost for the system processes and its products for system improvement. Tsatsaronis and Pisa (1994) conducted an exergoeconomic evaluation of the CGAM problem (Valero et al., 1994). This is a predefined problem of the gas turbine engine. It shows that the exergoeconomic concept is a powerful tool in the determination of the cost sources and for the optimization of the complex system. Hence the exergoeconomic technique is a very important tool for thermal system designers in the determination of thermodynamic inefficiencies and costs in the thermal system (Tsatsaronis, 1996). Abusoglu and Kanoglu (2009a, 2009b) conducted a review of the different Download English Version:

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