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Nonlinear dynamic analysis of a two-phase natural circulation loop with multiple nuclear-coupled boiling channels

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ABSTRACT

This study integrates the models developed previously by the authors to explore the stabilities, nonlinear dynamics and oscillation modes of a two-phase natural circulation loop with multiple nuclear-coupled boiling channels. The results indicate that both the pure thermal-hydraulic and nuclear-coupled boiling systems indeed have two instability regions, i.e. type-I and type-II instabilities, respectively. The pure thermal-hydraulic system tends to present in-phase mode of oscillations at the type-I boundary states and, in general, out-of-phase oscillations along with the type-II stability boundary. The oscillation modes may be affected by the configuration of parallel channels. By introducing the void-reactivity feedback together with neutron interaction, the coupling thermal-hydraulic and nuclear effects would induce complex influences on the system stability as well as the nonlinear oscillation modes. The in-phase mode, instead of out-of-phase mode, majorly dominates over the type-II boundary as the neutronic feedback is increased through void-reactivity coefficient. The complex nonlinear phenomena, such as complex periodic and chaotic oscillations, may appear in this multi-channel nuclear-coupled boiling natural circulation loop subject to a strong void-reactivity feedback ($3C\alpha$) coupled with a weak subcore-to-subcore neutron interaction ($\epsilon_{ij} = 7.0$).

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1. Introduction

Many advanced designs benefiting from the experience accumulated with the current plants are adopted by the advance boiling water reactors (ABWRs). Natural circulation is an important passive heat removal mechanism for an ABWR during the startup and shutdown processes. The boiling natural circulation system may be susceptible to different types of instability, i.e. static and dynamic instabilities. Density wave oscillations (DWOs) are a typical type of dynamic instability occurring in the boiling system (Boure et al., 1973). The stability issues of DWOs in two-phase natural circulation systems are very crucial to their safe operations.

Most two-phase flow systems consist of multiple parallel boiling channels, which channel-to-channel interactions can distribute over the channels. The studies concerning DWOs combined with parallel channel instability are of significant interest. Guido et al. (1991) indicated that in-phase and out-of-phase oscillations were the fundamental oscillation modes for an identical double channel system. Podowski et al. (1990) revealed complex interaction

modes involving coupled parallel channels caused by the differences among the channels. Lee and Pan (1999) reported that complex channel-to-channel interactions might drive the system more unstable with increasing number of channels. The oscillations among channels were essentially out-of-phase in the multi-channel system having a constant force circulation flow rate. This meant that out-of-phase instability could appear in such a system. Moreover, the out-of-phase oscillations could be identified in a parallel twin-channel experimental system with uniform and non-uniform heating powers at given flow rates (Guo et al., 2010). Xia et al. (2012) observed that four types of instability, i.e. Ledinegg instability, Ledinegg inducing out-of-phase instability, in-phase and out-of-phase instabilities, might exist in a relative low-pressure parallel narrow multi-channel system.

A natural circulation loop has two major types of instability (Fukuda and Kobori, 1979), i.e. type-I instability in the low power region caused by the gravitational pressure drop and type-II instability in the high power region dominated by the two-phase frictional pressure drop. In a natural circulation system, the system flow rate will depend on the system geometries and the operating parameters, such as the heating power and inlet subcooling. The nonlinear oscillation modes among parallel channels could be

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Nomenclature

A	area (m^2)		
A_H	total cross sectional area of multiple heated channels (m^2)	u_{i0}	steady state inlet velocity (m s^{-1})
$A_{H,j}$	cross sectional area of the j -th heated channel (m^2)	u_s	velocity scale, = $1.62g^{0.569}D_H^{0.705}\nu^{-0.137}$ (Jeng and Pan, 1994)
C_j	dynamic precursor concentration in j-th subcore ($\#\text{m}^{-3}$)	u^+	non-dimensional velocity, $=u/u_s$
C_{j0}	steady state precursor concentration in j-th subcore ($\#\text{m}^{-3}$)	v_f	specific volume of saturated liquid ($\text{m}^3 \text{kg}^{-1}$)
C_j^+	non-dimensional precursor concentration in j-th subcore, $=(C_j - C_{j0})/C_{j0}$	v_{fg}	difference in specific volume of saturated liquid and vapor ($\text{m}^3 \text{kg}^{-1}$)
C_D	Doppler-reactivity coefficient ($\$/\Delta T_F$)	V	volume (m^3)
C_{pf}	liquid constant pressure specific heat ($\text{J kg}^{-1} \text{K}^{-1}$)	W	mass flow rate (kg s^{-1})
C_α	void-reactivity coefficient ($\$/\%$)	W^+	non-dimensional mass flow rate, $=W/\rho_f A_H u_s$
D	diameter (m)	x	quality
f	friction factor	z	axial coordinate (m)
$f_{1\phi}$	single-phase friction factor	z^+	non-dimensional axial coordinate, $=z/L_H$
$f_{2\phi}$	two-phase friction factor		
Fr	Froude number, $=u_s^2/gL_H$	Greek symbols	
H_{jm}	interaction coefficient between subcores	α	void fraction or thermal diffusivity
h	heat transfer coefficient ($\text{W m}^{-2} \text{K}^{-1}$) or enthalpy (J kg^{-1})	β	delayed neutron fraction
h_c	clad-to-coolant heat transfer coefficient ($\text{W m}^{-2} \text{K}^{-1}$)	e_{jm}	neutron interaction parameter between subcores
h_f	saturated liquid enthalpy (J kg^{-1})	ν	kinematic viscosity (m^2/s)
h_{fg}	latent heat of evaporation (J kg^{-1})	ΔP	pressure drop (Pa)
h_g	saturated vapor enthalpy (J kg^{-1})	ΔP^+	non-dimensional pressure drop, $=\Delta P/\rho_f g L_H$
h_{gap}	Pellet-to-clad gap conductance ($\text{W m}^{-2} \text{K}^{-1}$)	δx	($x - x_0$) for variable x , x_0 represents the steady-state value
h_i	inlet liquid enthalpy (J kg^{-1})	ρ	density (kg m^{-3}) or reactivity ($\Delta K/K$, where K is multiplication factor)
h_s	enthalpy scale, $=Q_0/\rho_f A_H u_s$	ρ^+	non-dimensional density, $=\rho/\rho_f$
h^*	non-dimensional liquid enthalpy, $=(h-h_f)/h_s$	ρ_f	density of saturated liquid (kg m^{-3})
k	thermal conductivity($\text{W m}^{-1} \text{K}^{-1}$) or loss coefficient	Λ	friction number or neutron generation time (s)
L	length (m)	$\Lambda_{1\phi}$	single-phase friction number, $=f_{1\phi}L/2D$
L_H	channel length (m)	$\Lambda_{2\phi}$	two-phase friction number, $=f_{2\phi}L/2D$
L^+	non-dimensional length, $=L/L_H$	λ	boiling boundary (m)
M	mass (kg)	λ^+	non-dimensional boiling boundary, $=\lambda/L_H$
M^+	non-dimensional mass, $=M/\rho_f L_H A_H$	λ_C	decay constant of delayed neutron precursor (s^{-1})
N_j	dynamic neutron density in j-th subcore ($\#\text{m}^{-3}$)	Subscripts	
N_{j0}	steady state neutron density in j-th subcore ($\#\text{m}^{-3}$)	ch	channel
N_R	number of nodes in the riser	C	cladding
N_s	number of nodes in the single-phase region of the heated channel	e	exit of heated channel
N_{pch}	average steady-state phase change number	ex	exit
$N_{pch,j}$	steady-state phase change number for j-th channel, $=Q_{j0}/(\rho_f A_{H,j} u_s h_{fg}) \times v_{fg}/v_f$	f	saturated liquid
N_{sub}	subcooling number, $=(h_f-h_i)/h_{fg} \times v_{fg}/v_f$	fw	feedwater
N_j^+	non-dimensional neutron density in j-th subcore, $=(N_j - N_{j0})/N_{j0}$	F	fuel pellet
P	system pressure (bar)	g	saturated vapor
Q_j	heating power in j-th channel (W)	H	heated channel
Q_{j0}	steady-state heating power in j-th channel (W)	i	inlet of heated channel
Q_0	average steady-state heating power (W)	in	inlet
q''	heat flux (W m^{-2})	ld	lower downcomer
q_0''	steady state heat flux (W m^{-2})	lp	lower plenum
q''^+	non-dimensional heat flux, $=q''/q_0''$	mix	mixed flow
q'''	volumetric heat generation rate (W m^{-3})	j	j-th channel or subcore
r	radius (m)	n	n-th node in the single-phase region
Re	Reynolds number, $=uD/\nu$	r	r-th node in the riser
T	temperature (K)	R	riser
T_0	steady-state heated wall temperature (K)	sep	steam separator
T_{sat}	saturation temperature (K)	tot	total
T^*	non-dimensional temperature, $=(T - T_0)/T_{sat}$	ud	upper downcomer
t	time (s)	up	upper plenum
t_{ref}	time scale, $=L_H/u_s$	1ϕ	single-phase
t^*	non-dimensional time, $=t/t_{ref}$	2ϕ	two-phase
		0	steady state

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