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Viljami Maakala, Mika Järvinen, Ville Vuorinen

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Optimizing the Heat Transfer Performance of the Recovery Boiler Superheaters Using Simulated Annealing, Surrogate Modeling, and Computational Fluid Dynamics

Viljami Maakala^{a,*}, Mika Järvinen^b, Ville Vuorinen^b

^aAndritz, Helsinki, Finland

^bAalto University, Department of Mechanical Engineering, Espoo, Finland

*Corresponding author. Email: viljami.maakala@andritz.com

Abstract

The energy efficiency of recovery boiler power plants is largely influenced by the heat transfer to the superheaters. In the design process of such very large-scale applications, one of the key challenges is the a priori geometry optimization by robust numerical approaches. The main objectives of this work are to demonstrate a numerical optimization framework and to optimize the geometry of the superheater region to enhance the heat transfer. The framework is implemented as a surrogate-based optimization method, which combines simulated annealing, local polynomial regression, and computational fluid dynamics. The novelty of this work consists of the following: 1) The optimization framework is designed and introduced. 2) The connection between the geometry and heat transfer is quantified by formulating the optimal design curve. 3) The optimal design for a typical, existing recovery boiler is identified. The results indicate that the uniformity of the flow field is improved, and the heat transfer rate is increased by 5%. 4) The results indicate the importance of minimizing the separation vortices through the geometrical design with a strong linkage to the overall heat transfer rate. 5) The potential of optimization methods in this very large-scale energy production application is demonstrated for the first time.

Keywords: heat transfer, energy efficiency, optimization, recovery boiler, computational fluid dynamics, surrogate modeling

CFD model	
$D_{n,\mathrm{eff}}$	effective diffusivity of species $n [m^2/s]$
e _{mean}	mean absolute error of the heat transfer rates to the SHs [%]
e _{total}	error in the total heat transfer rate to the SHs [%]
f	body force vector [N]
g	gravitational acceleration vector [m/s ²]
GCI _{total}	discretization error estimate for the total heat transfer rate to the SHs [%]
h	sensible enthalpy [J/kg]
h _{desh}	enthalpy of the desuperheating water [J/kg]
h_n	sensible enthalpy of species n [J/kg]
$h^i_{ m bef}$	enthalpy of the steam before SH <i>i</i> before desuperheating [J/kg]
$h_{ m in}^i$	enthalpy of the steam at the inlet of SH <i>i</i> after desuperheating [J/kg]
$h_{ m out}^i$	enthalpy of the steam at the outlet of SH <i>i</i> [J/kg]

Nomenclature

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