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Monitoring of thermal stresses in pressure components based on the wall temperature measurement

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ABSTRACT

Thick-wall boiler components limit maximum heating and cooling rates during start-up or shut-down of the boiler. First, the allowable heating rates of the critical pressure components of the boiler were determined, and the temperature of the fluid was determined. The rate of change of the wall temperature of the pressure element and the thermal stress on the inner surface are controlled online and compared with the permissible values. Boiler manufacturers designate thermal stresses on the inner surface of the pressure component on the edge of the hole based on the measurement of the wall temperature at two points located inside it. Due to the low accuracy of the method used by boiler manufacturers, a new stress-determination method has been proposed in this paper in which only the internal temperature measurement point is used to determine the stresses on the inner surface of the component. In the method proposed in the paper, first, the internal surface temperature is determined from the inverse heat conduction solution, and then the stresses are calculated. Numerous computational tests were performed for cylindrical and spherical elements. Thermal stresses on the inner surface were also determined based on actual measurement data. Thermal stresses can be monitored at small time intervals. The advantage of the method is its high accuracy even at rapid changes in the fluid temperature.

1. Introduction

A mixed structure characterizes the contemporary energy system. In addition to thermal, classical or nuclear power plants, wind farms, photovoltaic cells, and other renewable energy sources are also important [1]. Buttler et al. [1] measured time series of wind power, solar power and load of the year 2014 to identify the current challenges of the integration of wind and solar power in the electricity system of the EU (European Union). Big changes in power output are typical for wind and solar power. More flexibility is therefore demanded from classic thermal blocks [2–5]. Four different types of conventional power plants were investigated in Ref. [2] for different options with increasing CO₂ and fuel prices to determine the impact of different flexibility solutions. In Ref. [3], a computer simulation of a steam-gas power unit with a Benson once-through boiler was performed to study the fast gas turbine

start-up (within 20 min) on the dynamic behavior of a Benson heat recovery steam generator. A dynamic sub-critical Benson HRSG (Heat Recovery Steam Generator) model was developed using the commercial software "Advanced Process Simulation Software" (APROS) [3]. Hentschel et al. [4] carried out the detailed modeling of a hard coal-fired power plant using the thermos-hydraulic simulation code APROS to improve the boiler flexibility. A review of programmes for dynamic simulation of thermal power plants for such as ASPEN PLUS DYNAMICS, DYMOLA and APROS were conducted in Ref. [5]. Combined steam and gas, pulverized coal, and nuclear power units were simulated using various codes.

The subject of the present work is closely related to the improvement of the flexibility of thermal power plants. In connection with the development of wind farms, characterized by high variability of generated power over time, thermal steam blocks must be quickly started and switched off, so that the power supply in the system and its demand by the recipients are equal. For this reason, the time of start-ups and shut-downs of the boiler should be as short as possible, while maintaining safe and longterm boiler operation. Determining the allowable heating and





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Nomenclature		α_p	stress concentration factor for circumferential stress
			due to pressure
		β	linear thermal expansion coefficient, 1/K
Symbols _{Cw}	specific heat capacity,]/(kg·K)	δ	distance of the temperature sensor from the inner surface of the component. m
d_{in}	inner diameter, m	δ1	distance of the temperature sensor from the outer
d_m	mean diameter, m	. 1	surface of the component. m
dout	outer diameter, m	Δr	radial step in the solution of direct heat conduction
E	Young's modulus, Pa		problem. m
f	wall temperature measured at the node 2 located at	Δr_1	radial step in the solution of direct heat conduction
-	the distance δ from the inner surface of the	1	problem, m
	component, °C	Δt	time step, s
G	wall temperature measured at the outer surface of	ΔT	initial jump in fluid temperature, °C or K
	the component, °C	Δt_s	sampling time of the wall temperature measurement,
FEM	Finite Element Method		S
FVM	Finite Volume Method	$\varepsilon_T, \varepsilon_\sigma$	relative error of temperature and stress
Fo	Fourier number, $Fo = \kappa_w t/s^2$		determination at inner surface, %
Fo*	Fourier number after which the quasi-steady state is	$\varepsilon_1, \varepsilon_2$	relative errors, %
	formed, $Fo^* = \kappa_w t^* / s^2$	ν	Poisson's ratio
h	heat transfer coefficient, $W/(m^2 \cdot K)$	$ ho_w$	density, kg/m³
k_w	thermal conductivity, W/(m·K)	σ_T	circumferential thermal stress, MPa
N	number of control volumes in the radial direction	σ_T'	circumferential thermal stress given by Eq. (20), MPa
т	the parameter in heat conduction equation ($m = 1$ for	$\sigma_T^{''}$	circumferential thermal stress given by Eq. (21), MPa
	the cylindrical wall, $m = 2$ for the spherical wall)	σ_T^2	variance of pseudo-random errors
р	pressure, Pa	σ_{al}	allowable stress, MPa
$P_1,P_2,\ P_3$	points on the inner surface of the pressure element	σ_p	circumferential stresses caused by pressure, MPa
	on the edge of the opening	σ_{φ,P_i}	circumferential stress at point P _i , MPa
r_c	mean radius, $r_c = (r_{in} + r_{out})/2$, m	ϕ	shape factor
r _{in}	inner radius of the component, m	κ _w	thermal diffusivity, m ² /s
r_m	radius of the point at which the wall temperature	∇	gradient operation (nabla)
DMCE	equals the average temperature, in		
RIVISE	outer radius of the component m	Subscripts	
r _{out}	radius at with the temperature sensor is located m	al	allowable
rs s	will thickness m	C .	center
5 t	time s	dır	direct solution
t t*	time, s	in	inner
ι Τ	temperature °C or K	inv	inverse solution
T Ta	temperature, conk temperature measured in the center of the wall °C or	m	nominal
10	K	nom	nonnal
Teo	initial fluid temperature. °C or K	oui n	Draccura
T _f	fluid temperature. °C or K	р D	pressure
T1 T	S_{max} wall temperature at nodes 1.2, and 3. °C or K		thermal
$T_W^{1,1}W^{2,1}$	wall temperature. °C or K	1	wall
	measured wall temperature. °C or K	0	initial
T _w m	mean temperature on the wall thickness. °C or K	Ø	circumferential
u	the ratio of the outer to the inner radius, $u = r_{out}/r_{in}$	Ŧ	
VT	rate of temperature variation, K/s	Superscripts	
•	· · · ·	m	measured
Greek syn	abols	п	number of time step
α_T	stress concentration factor for circumferential	*	beginning of a quasi-steady state
	thermal stress		

cooling rates of critical boiler pressure elements is, therefore, crucial to shortening the boiler start-up and shut-down operations. It is also necessary to develop a method for monitoring the rate of temperature changes of the critical element walls of the boiler and monitoring thermal stresses on their internal surface so that during the boiler operation, instantaneous heating and cooling rates and thermal stresses do not exceed the allowable values. Combined - cycle power plants are increasingly used in power systems with a

high share of renewable energy because of their better flexibility [6-10]. Different aspects of cycling operation of combined cycle power plants were investigated.

During the starts, shutdowns and load changes of steam boilers, thick-walled pressure components of complex shape are subjected to rapid temperatures variations and high thermal stresses. The critical pressure components such as the drum, steam-water separator, inlet and outlet headers of the superheaters stages, Download English Version:

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