



Model of a thermal driven volumetric pump for energy harvesting in an underwater glider



J. Falcão Carneiro*, F. Gomes de Almeida

INEGI, Faculdade de Engenharia, Universidade do Porto, Rua Dr. Roberto Frias, s/n, 4200-465, Porto, Portugal

ARTICLE INFO

Article history:

Received 14 May 2015
Received in revised form
2 June 2016
Accepted 3 June 2016

Keywords:

Underwater gliders
Renewable energy
Energy efficiency
Thermodynamic cycle
Hydraulic systems
Phase change materials

ABSTRACT

Underwater gliders are one of the most promising approaches to achieve an increase of human presence in the oceans. Among existing solutions, thermal driven gliders present long range and endurance capabilities, offering the possibility of remaining years beneath water collecting and transmitting data to shore. A key component in thermal gliders lies in the process used to collect ocean's thermal energy. In this paper a new quasi-static model of a thermal driven volumetric pump, for use in underwater gliders, is presented. The study also encompasses an analysis of the influence different hydraulic system parameters have on the thermodynamic cycle efficiency. Finally, the paper proposes a simple dynamic model of a heat exchanger that uses commercially available materials for the Phase Change Material (PCM) container. Simulation results validate the models developed.

© 2016 Elsevier Ltd. All rights reserved.

1. Introduction

In order to widen the knowledge on Earth's oceans and its underlying resources, a more persistent human presence on and under water is required. However, common techniques based on ships or buoys are currently expensive and do not allow the acquisition of data with an adequate spatial and temporal resolution. It is therefore vital to develop compact, smart and low cost devices that allow the creation of constantly monitoring networks. This scenario has led, in recent years, to an exponential increase in the number of studies involving Autonomous Underwater Vehicles (AUV) [1]. Furthermore, this trend has pushed AUV technology to evolve from concept demonstrators to commercially available products [1].

One particularly well suited type of AUV for collecting ocean data is the underwater glider. This AUV type uses buoyancy changes as propeller mean, therefore leading to very low energy consumptions. Furthermore, given its natural sawtooth trajectory profile, it allows collecting data along the water column, a fact of major importance regarding biological data acquisition [2].

Glidors were originally proposed and developed as inexpensive remote sensing systems for oceanographic purposes and have

recently also been considered for sovereignty upholding tasks [3]. Data gathered by these vehicles can be used in data assimilation procedures and to calibrate circulation models, e.g. Refs. [4,5]. The energy expended by these vehicles is mostly used in buoyancy changes, and can reach as much as 80% [3] in electrically powered pumping procedures. Presently there are several proposals to tackle the problem, some aim to use the waste heat from internal systems [6], while others aim to completely remove the need for significant pre-installed energy and are based on the conversion of environmental energy, like the use of the ocean thermal gradient (OTG) [7]. There are also other types of vehicles using environmental energy like solar energy [8] or solar energy combined with a wave energy conversion mechanism [9]. The use of solar [8] or wave powered [9] devices in this context suffers a major drawback, as these devices must spend most of their time at sea surface. This means that a vehicle, in the absence of survival maneuvering capability, which has been the case for most, will be subject to storms, strong waves and winds which may lead to decreased operational life. On the contrary, collecting energy from the sea temperature differences provides a safer travelling environment since none of the above mentioned natural activity is present underwater. Within the context of autonomous vehicles, the ocean's thermal energy is typically collected by converting the volumetric expansion, or contraction, that some type of materials (Phase Change Materials, PCM) present when changing from solid to liquid phase and vice

* Corresponding author.

E-mail address: jpbrfc@fe.up.pt (J. Falcão Carneiro).

Notation

$(\circ)_{SL}$ variable at solidus line
 $(\circ)_{LL}$ variable at liquidus line
 C_{HE} specific heat of the heat exchanger
 C_{PCM} represents the specific heat capacity of the PCM
 C_{HE} thermal capacity of the heat exchanger
 C_{PCM} thermal capacity of the PCM
 $\bar{C}_{PCM_{S_i S_j}}$ average value of the PCM heat capacity when travelling from S_i to S_j
 C_p specific heat at constant pressure
 $C_{p_PCM,s}$ PCM specific heat at constant pressure for solid phase
 $C_{p_PCM,l}$ PCM specific heat at constant pressure for liquid phase
 C_v specific heat at constant volume
 $C_{v_PCM,s}$ PCM specific heat at constant volume for solid phase
 $C_{v_PCM,l}$ PCM specific heat at constant volume for liquid phase
 CV_i check valve i
 E_{HE} Young modulus of the heat exchanger material
 K thermal conductivity of the PCM
 k_i auxiliary variable thermal conductivity of the PCM at either solidus or liquidus lines
 k_L thermal conductivity of the PCM in the liquid phase
 k_S thermal conductivity of the PCM in the solid phase
 k_{LL} thermal conductivity of the PCM at liquidus line
 k_{SL} thermal conductivity of the PCM at solidus line
 H enthalpy of the PCM
 h specific enthalpy of the PCM
 h_i auxiliary variable: enthalpy at either solidus or liquidus lines
 h_{LL} enthalpy at liquidus line
 h_{SL} enthalpy at solidus line
 L_{HE} length of the heat exchanger tubes
 M_{HE} mass of the heat exchanger
 M_{PCM} mass of the PCM
 p_{N2}^i N_2 pressure at state i
 p_{N2}^{max} thermodynamic cycle maximum pressure of the PCM
 $p_{oil-PCM}$ pressure at $V_{oil-PCM}$
 p_{oil-N2} pressure at V_{oil-N2}
 p_{PCM} PCM pressure
 p_{PCM}^{max} maximum PCM pressure
 PP auxiliary variable defining the phase of the PCM before the transition phase
 p_t tank pressure
 Q_f PCM the heat of fusion at atmospheric pressure
 Q_{PCM_in} heat retrieved from the surrounding water by the heat exchanger
 $Q_{PCM_{S_i S_j}}$ heat exchanged by the PCM with the environment when travelling from S_i to S_j
 r_{ext_HE} external radius of the heat exchanger cylinder
 r_{inter_HE} intermediate radius of the heat exchanger cylinder
 r_{int_HE} internal radius of the heat exchanger cylinder
 r_{ext_PCM} external radius of the PCM cylinder
 r_{inter_PCM} intermediate radius of the PCM cylinder
 r_{int_PCM} internal radius of the PCM cylinder
 R_{H2O_HE} heat transfer convective resistance between water and heat exchanger
 R_{HE} total heat transfer conductive resistance of the HE
 R_{HE_EXT} heat transfer conductive resistance between water and T_{HE}
 R_{HE_INT} heat transfer convective resistance between T_{HE} and the outer layer of the PCM
 R_{PCM} total heat transfer conductive resistance of the PCM
 R_{cond} conductive heat transfer resistance

R_{conv} convective heat transfer resistance
 S set of possible states the PCM experiences
 S state of the PCM
 S_i state i of the PCM
 S_i^* notable state i of the PCM
 $(S)^{-1}$ previous state of the PCM on the state trajectory evolution
 S_{ij} set of states the PCM undergoes when travelling from S_i to S_j
 S_{inter} generic intermediate state of the PCM between S_i and S_j
 V_{PCM} PCM specific volume of the PCM
 V_{N2}^0 volume of the accumulator
 V_{N2}^{min} volume of gas at the accumulator when $p_{N2} = p_{N2}^{max}$
 $V_{oil-PCM}$ volume of oil between the PCM, CV_1 and CV_2
 $V_{oil-PCM}^i$ $V_{oil-PCM}$ at state i
 V_{oil-N2} volume of oil between CV_1 and the accumulator bladder
 V_{PCM} volume of the PCM
 V_f fixed volume comprising $V_{oil-PCM}$ and V_{PCM}
 t thickness of the heat exchanger tube
 t_{MTS} minimum thickness of the heat exchanger tube according to the MTS criteria
 t_{CBC} minimum thickness of the heat exchanger tube according to the CBC criteria
 T_c lower ocean temperature
 $T_{F,L}$ temperature at which the PCM melting process ends.
 $T_{F,S}$ the temperature at which the PCM melting process starts
 $T_{F,M}$ temperature at which the middle stage of the PCM melting process is reached
 T_h ocean temperature on surface
 T_{HE} heat exchanger temperature at an intermediate radius
 T_i auxiliary variable: temperature at either solidus or liquidus lines
 T_{LL} temperature of the PCM at liquidus line
 T_{LL}^i temperature of the PCM at liquidus line when the PCM is at state i
 T_{PCM} PCM temperature (at a radius corresponding to half the total volume of the PCM cylinder)
 T_{PCM}^i PCM temperature at state i
 T_{SL} temperature of the PCM at solidus line
 T_{SL}^i temperature of the PCM at solidus line when the PCM is at state i
 U internal energy of the PCM
 u specific internal energy of the PCM
 v_v vertical velocity of the glider
 z ocean water depth
 W_{N2} work performed during the cycle over the gas accumulator
 α thermal volumetric expansion coefficient of the PCM
 $\beta_{e,oil}$ effective isothermal bulk modulus of oil
 Δk absolute difference between the thermal conductivity of the PCM at solidus and liquidus lines
 ΔT_t absolute difference between T_{SL} and T_{LL}
 θ convective heat transfer coefficient between sea water and heat exchanger
 κ compressibility coefficient of the PCM
 ϕ external diameter of the heat exchanger tubes
 η efficiency of the cycle
 η_{max} maximum cycle efficiency
 η_{max_c} maximum efficiency of the thermal driven volumetric pump (Carnot corollary)

Download English Version:

<https://daneshyari.com/en/article/8072926>

Download Persian Version:

<https://daneshyari.com/article/8072926>

[Daneshyari.com](https://daneshyari.com)