



Residual trapping of carbon dioxide during geological storage—Insight gained through a pore-network modeling approach



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ABSTRACT

To reduce emissions of the greenhouse gas CO₂ to the atmosphere, sequestration in deep saline aquifers is a viable strategy. Residual trapping is a key containment process important to the success of CO₂ storage operations. While residual trapping affects CO₂ migration over large scales, it is inherently a pore-scale process. Pore-network models (PNMs), capturing such processes, are useful for our understanding of residual trapping, and for upscaling trapping parameters for larger scale models. A PNM for simulation of quasi-static two-phase flow; CO₂ intrusion (drainage) followed by water flooding (imbibition) was developed. It accounts for pore-scale displacement mechanisms, and was used to investigate residual CO₂ trapping. The sensitivity of the residual CO₂ saturation to several parameters was studied, to validate a trapping behavior in agreement with earlier studies. Then the PNM was calibrated to core sample data and used to simulate drainage-imbibition scenarios with different turning point saturations. From these the initial-residual saturation curves of CO₂ in Heletz sandstone were estimated, essential for future macroscopic-scale simulations. Further, the occurrence of different pore-scale mechanisms were quantified and the size distribution of the residual trapping clusters was shown to exhibit a bimodal appearance. The findings improve the understanding of residual trapping in Heletz sandstone.

1. Background

1.1. Introduction

Geological storage of carbon dioxide (CO₂) in deep saline aquifers is one approach to mitigate greenhouse gas release from point sources to the atmosphere. The sequestered CO₂ is held in the subsurface by several trapping mechanisms, including structural and stratigraphical trapping, solubility trapping, geochemical trapping and residual trapping (IPCC, 2005). This study addresses residual trapping, which occurs when the stored CO₂ is displaced by formation fluid, as is the case at the trailing edge of a buoyantly migrating carbon dioxide plume (Ide et al., 2007; Kumar et al., 2005) or if chase-brine is used in the injection-design (Qi et al., 2009). Blobs or ganglia of CO₂ can then be disconnected from the plume and immobilized by capillary forces (Ide et al., 2007). The residual trapping gives rise to hysteresis in the characteristic functions: relative permeability and capillary pressure functions. The effect of hysteresis in relative permeability, on geological CO₂ storage has been evaluated through numerical simulations of storage scenarios (Doughty, 2007; Doughty and Myer, 2009; Flett et al.,

2004; Juanes et al., 2006; Spiteri et al., 2005). These studies indicate that residual trapped CO₂, may comprise a substantial part of the stored CO₂ and provide secure storage. An in-depth understanding of the mechanisms and processes influencing the residual trapping of CO₂ is therefore of great importance.

The CO₂ saturation at which immobilization through capillary trapping occurs is referred to as the residual CO₂ saturation or residual gas saturation (S_{gr}). For brevity the CO₂-rich phase is referred to here as the gas phase, although technically in this case the CO₂ is in its supercritical state. The maximum residual gas saturation (S_{grmax}) is the residual gas saturation obtained after a rock has undergone complete imbibition by water from an initial state where the water saturation is at its irreducible saturation. Residual trapping of supercritical carbon dioxide in sandstone, a common rock found in basins used for CO₂ storage, has been reported in the saturation range of 0.087–0.35 (Andrew et al., 2014; Bennion and Bachu, 2008a; Iglauer et al., 2011; Krevor et al., 2012; Pentland et al., 2011; Rahman et al., 2016; Shi et al., 2011; Suekane et al., 2008; Zuo and Benson, 2014). A study by Hamon et al. (2001) of gas (not only CO₂) trapping in heterogeneous sandstones found that the S_{grmax} ranged from 0.05 to 0.85. For gases in

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Nomenclature			
A	Area	scCO ₂	Supercritical CO ₂
AM	Arc meniscus	v_s	Velocity
Bo	Bond number ($=\Delta\rho g a^2/\sigma$)	V_g^i	Volume of i:th ganglion
CO ₂	Carbon dioxide	$w^{(x)}$	Parametric weight taking into account the effect of geometry
CCS	Carbon capture and storage	W	Random number
cpb	Cooperative pore body filling	z	Coordination number
EOR	Enhanced oil recovery	\bar{z}	Mean coordination number
G	Shape factor ($=\text{Area}/\text{Perimeter}^2$)	<i>Greek letters</i>	
g	Gravitational acceleration	β_i	Corner half angle
$g_{i,II}$	Effective hydraulic conductance of phase i	Δ	Difference
h	Vertical distance from z = 0.0 to the element	$\Delta\rho$	Density difference between phases
I_n	Cooperative pore body filling event n	θ	Contact angle
k	Absolute permeability	μ	Viscosity
k_{rx}	Relative permeability of phase x	σ	Interfacial tension between the wetting phase and the non-wetting phase
l_{ij}	Length of pore throat between pore body i and pore body j	τ	Tortuosity
$L_{body\ centers}$	Distance between body centers	<i>Superscript</i>	
M	Viscosity ratio, mobility ratio ($=\mu_{inv}/\mu_{def}$)	e	Entry
MTAM	Main terminal arc meniscus	element	Element (throat or body)
n	Number of corners	pd	Piston-type displacement
N_c	Capillary number ($=\mu_{inv}q_{inv}/\sigma$ or $=\mu_{nw}u_{nw}/(\sigma \times \cos\theta)$)	so	Snap-off
P	Pressure	<i>Subscript</i>	
P_c	Capillary pressure	a	Advancing
P_c^e	Capillary entry pressure	a,max	Maximum advancing
$P_{c,n}^e$	Threshold capillary pressure for an I_n -cpb-filling event	c	Capillary
$P_{c,PISTON}^e$	Threshold capillary pressure for piston-type displacement	def	Defending fluid
$P_{c,so}^e$	Threshold capillary pressure for snap-off	g	Gas phase, here scCO ₂
P_c^{max}	Highest capillary pressure during drainage	h	Hinging
P_c^{trap}	Capillary pressure at which trapping occurred	inv	Invading fluid
PNM	Pore-network model	nw	Non-wetting
q	Darcy velocity	o	Oil
$q_{i,II}$	Flow rate of phase i between pore body I and pore body J	r	Receding
Q_{tot}	Total flow rate	scCO ₂	Supercritical CO ₂
r	Radius	t	Throat
\bar{R}_n	Average radius of curvature for an I_n -cooperative pore body-filling event	w	Wetting
REV	Representative elementary volume		
S_{xi}	Initial saturation of phase x at the start of imbibition		
S_{xr}	Residual saturation of phase x		
S_{gmax}	Maximum residual gas saturation		
SSORCG	Symmetric successive overrelaxation – preconditioned conjugate gradients		

general, not limited to CO₂, S_{gr} has been shown to depend on the porosity (/permeability), microporosity and initial gas saturation at the start of imbibition (S_{gi}) (Suzanne et al., 2003). Residual trapping of CO₂ is also dependent on the wettability of the medium and shape of the grains (Chaudhary et al., 2013). It also increases with interfacial tension (σ) (Bennion and Bachu, 2006). The σ is in turn dependent on the temperature, pressure and salinity conditions (Chalbaud et al., 2006; Bennion and Bachu, 2006, 2008b). However, results from laboratory core flooding experiments indicate that pressure, temperature and salinity may have insignificant effect on the trapping curve, S_{gr} - S_{gi} relationship, of CO₂ in sandstone (Niu et al., 2015). The magnitude of S_{gr} also depends on the state of the CO₂; whether the CO₂ is supercritical or gaseous. For the CO₂/brine system, brine is more wetting in contact with gaseous CO₂ than in contact with supercritical CO₂, resulting in less capillary trapping in the latter case (Akbarabadi and Piri, 2013; Prather et al., 2016). Whether the CO₂-rich phase prior to imbibition originates from injected or exsolved phase also affects the residual CO₂ trapping, i.e. a process-dependency exists. The latter case results in greater trapping, explained by that in this case the CO₂ appears in a more uniform distribution in the heterogeneous media (Zuo and

Benson, 2014).

Numerical simulations are an important part of the planning and design stage of any storage project. While capillary trapping occurs at the pore-scale, there is a need to quantify residual trapping on the macroscopic scale. Trapping on the macroscopic scale, where Darcy-type flow is assumed, is of interest when simulating field-scale CO₂ storage, and is accounted for by using a trapping model (or an initial-residual saturation curve (IR curve)). Several trapping models, i.e. S_{gr} - S_{gi} relationships, of interest for gas trapping in sandstone were recounted and evaluated by Suzanne et al. (2003). There are multiple ways to obtain a trapping model. One approach is through fitting of a function to direct measurements. Experimentally measured trapping curves, S_{gr} - S_{gi} relationships, for supercritical and/or gaseous CO₂ in sandstone have been presented in several studies (Akbarabadi and Piri, 2013; Li et al., 2015; El-Maghraby et al., 2011; Pentland et al., 2011; Ruprecht et al., 2014). Another approach is to fit a function to data retrieved from pore-network modeling (Spiteri et al., 2005). Spiteri et al. (2005) used pore-network model simulations to derive and validate a hysteretic relative permeability function and trapping model. This approach made it possible to account for wettability conditions

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