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Influence of carbon to nitrogen ratio on nitrous oxide emission in an Integrated Fixed Film Activated Sludge Membrane BioReactor plant



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ABSTRACT

In this study a University of Cape Town (UCT) Integrated Fixed Film Activated Sludge (IFAS) Membrane BioReactor (MBR) wastewater treatment plant was monitored in terms of nitrous oxide (N₂O) emissions. The short term effect on the N₂O emission due to the influent carbon-to-nitrogen (C/N) ratio variation (C/N ratios of 2, 5 and 10 gCOD/gN) was evaluated. Since in a previous study, the effect of the C/N ratio was studied in the same system without biofilm (UCT-MBR configuration) the main aim here was to investigate the role of biofilms on N₂O emissions. Under all the investigated C/N ratios, the N₂O fluxes and the average emission factors were lower than that of previous studies with no biofilm presence. The total average N₂O emission was 0.5% of the influent nitrogen with biofilm (IFAS system) and 3.5% without biofilm. This result emphasizes the potential role of the biofilms in attenuating the N₂O emission sepecially in the case of stress conditions (i.e., low C/N influent ratios). An increase of N₂O fluxe from the anoxic reactor (till 28 mgN₂O m⁻²h⁻¹) occurred at the lowest influent C/N tested (2 gCOD/gN - phase III). At C/N equal to 2 gCOD/gN the anoxic reactor was the main source of N₂O, contributing 45% of all produced N₂O. This result was attributed to an incomplete denitrification caused by a lack of organic carbon and a slight increase of dissolved oxygen concentration.

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1. Introduction

During the last ten years, the interest towards greenhouse gas (GHG) emission from wastewater treatment plants (WWTPs) has increased considerably with the aim to design and operate plants that have the minimum environmental impact (Mannina et al., 2016a). In addition to the "traditional pollutants" such as organics compounds (indirectly measured by chemical oxygen demand - COD, biochemical oxygen demand - BOD₅), nitrogen - N or phosphorus – P, WWTPs can also emit GHGs (i.e., carbon dioxide – CO₂, methane – CH₄ and nitrous oxide – N₂O). GHGs can be emitted as a direct consequence of the biological processes (Mannina et al., 2016a) or indirectly due to the power requirements (Papa et al., 2016). Among the GHG emitted from WWTPs, N₂O has caused the greatest interest among scientist and researchers due to its high

global warming potential (GWP) (298 times higher than that of CO₂) (IPCC et al., 2013). N₂O from WWTPs is mainly produced by the biological nitrogen removal (BNR) processes through nitrification and subsequent denitrification both from autotrophic and heterotrophic bacteria (Kampschreur et al., 2009).

Ammonia oxidizing bacteria (AOB) have been identified as responsible of producing N₂O due to: i. the reduction of NO₂ as terminal electron acceptor to N₂O (AOB denitrification) (Kim et al., 2010); ii. the incomplete oxidation of hydroxylamine (NH₂OH) to NO₂ (Law et al., 2012). The predominance of AOB pathway to the other has not yet been demonstrated (Pocquet et al., 2016).

WWTP operating factors (such as, dissolved oxygen, C/N ratio, sludge retention time – SRT and temperature) may strongly influence the N₂O emission (Kampschreur et al., 2009). Stenström et al. (2014) have found that decreasing the oxygen concentration during nitrification lead to the increase of N₂O emission during the denitrification; similar results were also found by Frison et al. (2015). Recently, Mannina et al. (2017a) reported the effect of the influent C/N ratio on N₂O emissions from the same UCT- MBR pilot plant

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		NH₄Cl NH₄−N	ammonii ammonii
AOB	ammonia oxidizing bacteria	$NO_2 - N$	
ATU	Allylthiourea	-	nitrate n
b _н	endogenous decay coefficient	NOB	Nitrite O
BNR	biological nutrient removal	NO _x -N _{in}	influent
BOD	biochemical oxygen demand		permeat
BOD ₅	biochemical oxygen demand in five days	ODR	oxygen o
СŰ	carbon	ОНО	ordinary
$C_3H_8O_3$	glycerol	OP	ortho-P
CAS	conventional activated sludge	OUR	Oxygen
H ₃ COO	Na sodium acetate	Р	phospho
CH₄	methane	PAOs	phospha
CIP	clean in place	PHA	poly-β-h
20_{2}	carbon dioxide	P _{IN}	influent
COD	chemical oxygen demand	O ₄ -P	phospha
COD _{in}	influent COD	P _{OUT}	permeat
COD _{out}	permeate COD	Qairsi	volumet
COD _{SUP}	supernatant COD	SBR	sequenti
	total COD	SNDPR	simultan
D0	dissolved oxygen		phospho
DPAOs	denitrifying phosphate accumulating organisms	SRT	Sludge R
ECD	Electron capture detector	TKN	Total Kje
FA	free ammonia	TN	total niti
GC	Gas Chromatograph	TP	total pho
GHG	greenhouse gas	TSS	total sus
GWP	global warming potential	UCT	Universit
HRT	hydraulic retention time	VSS	volatile s
FAS	Integrated Fixed Film Activated Sludge	WWTPs	wastewa
K ₂ HPO ₄	dipotassium hydrogen phosphate	ηP_{TOT}	TP remo
MBBR	moving bed biofilm bioreactors	η_{BIO}	biologica
MBR	Membrane BioReactor	η _{denit}	denitrifie
N	nitrogen	η _{nit}	nitrificat
N ₂ O	nitrous oxide	ηP	OP remo
Nassimilati	on assimilated nitrogen	η _{тот}	total COI
	hydroxylamine	ηN_{total}	total niti
	influent nitrogen ammonia concentration	μ _{H.max}	heterotro
	tpermeate nitrogen ammonia concentration	(II,IIIaX	

NH₄Cl	ammonium chloride
	ammonium nitrogen
	nitrite nitrogen
	nitrate nitrogen
	Nitrite Oxidizing Bacteria
	influent nitrite and nitrate concentration
	t permeate nitrite and nitrate concentration
ODR	oxygen depletion reactor
ОНО	ordinary heterotrophic organism
OP	ortho-P
OUR	Oxygen Uptake Rate
Р	phosphorus
PAOs	phosphate accumulating organisms
PHA	poly-β-hydroxyalkanoates
P _{IN}	influent orthophosphate concentration
O ₄ -P	phosphate
Pout	permeate orthophosphate concentration
Qairi	volumetric gas flux
SBR	sequential batch rectors
SNDPR	simultaneous nitrification, denitrification, and
	phosphorus removal
SRT	Sludge Retention Time
TKN	Total Kjeldahl Nitrogen
TN	total nitrogen
TP	total phosphorus
TSS	total suspended solid
UCT	University Cape Town
VSS	volatile suspended solids
WWTPs	wastewater treatment plants
ηP _{TOT}	TP removal efficiency
η_{BIO}	biological COD removal efficiency
η _{denit}	denitrification efficiency
η_{nit}	nitrification efficiency
ηP	OP removal efficiency
η _{тот}	total COD removal efficiency
ηN_{total}	total nitrogen removal efficiency
$\mu_{H,max}$	heterotrophic growth rate

here discussed and, they found the highest N_2O emissions at the lowest investigated C/N ratio (5 gCOD/gN).

The variability of the influent features and of the used process configuration make the weight that each operating factor has on the total N₂O emission unknown. Such a fact leads, as a consequence, to a huge variability of the N₂O emission factors (with respect to the influent nitrogen load) available in the literature: 0.01-1.8% (Ahn et al., 2010; Rodriguez-Caballero et al., 2015), 0.036% (Aboobakar et al., 2013), 0.04-11% (Daelman et al., 2015).

Further, the existing difficulties in capturing and measuring the real overall N_2O produced from WWTPs (Marques et al., 2016) make data more case study specific and difficult to transfer to other systems (Mannina et al., 2016a).

Despite the knowledge on the N₂O emission from WWTP has considerably increased, it has been mostly acquired on conventional activated sludge systems (CAS) (Todt and Dörsch, 2016). Therefore, current knowledge may not directly be transferred into innovative systems such as MBR or moving bed biofilm bioreactors (MBBR or hybrid biological systems such as Integrated Fixed Film Activated Sludge –IFAS) Mannina et al. (2011). MBR systems as well as IFAS systems are characterized by specific peculiarities that would strongly influence the N₂O production/emission. For example, the intensive aeration for fouling mitigation in MBR can promote the N₂O stripping. Therefore, further studies to better understand how the peculiarities of MBR or IFAS systems influence the N₂O emissions are required.

With this regard, only few studies have been reported in literature. Todt and Dörsch (2016) found that the AOB denitrification and the incomplete heterotrophic denitrification as the main sources of N₂O production in biofilm systems. These two N₂O formation pathways occur mainly in hypoxic or anaerobic zone of biofilm, where the low O₂ concentration and the presence of NO₂ favor the N₂O formation.

Lo et al. (2010) demonstrated that from the hybrid system the production of N_2O was significantly higher (21.2% of the influent nitrogen) than that of pure biofilm systems (0.5% of the influent nitrogen) and suspended biomass systems (4.2% of the influent nitrogen).

Very recently, Kinh et al. (2017) have demonstrated that membrane-aerated biofilm reactor (MABR) provides lower N₂O emission than conventional biofilm reactor (CBR). Specifically, N₂O emission factor was 0.0058 \pm 0.0005% in the MABR and 0.72 \pm 0.13% in the CBR.

Studies on the quantification of N₂O from biofilm systems, such

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