



# Comprehensive literature review on CH<sub>4</sub>-CO<sub>2</sub> replacement in microscale porous media



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## ABSTRACT

Gas production studies from natural gas hydrate reservoirs have been the subject of extensive research in recent years. Although CH<sub>4</sub>-CO<sub>2</sub> replacement production method from gas hydrates has many advantages, the number of the studies related to this production method are less than depressurization production method studies, especially in microscale porous media. Hence, this paper presents a comprehensive literature review on CH<sub>4</sub>-CO<sub>2</sub> replacement to better understand the associated processes and mechanisms in microscale porous media with emphasis on micromodel experiments, 3D imaging, other visualization testing method and pore network modelling. Moreover, the advantages and disadvantages of currently available CH<sub>4</sub>-CO<sub>2</sub> replacement studies were investigated. The critical issues of the replacement method were underlined and new suggestions have been offered for future investigations.

## 1. Introduction

Unconventional energy resources have become very important in recent years due to the decline of conventional hydrocarbon reservoirs. Shale gas reservoirs and natural gas hydrates are the most common ones of the unconventional reservoirs in the world (Chong et al., 2016; Ritts, 2017). Feasible gas production from shale gas reservoirs is currently possible with the technological advancements in horizontal drilling and hydraulic fracturing operations. However, gas production from another unconventional gas reservoir, which is gas hydrate, is still immature and is in the stage of development (SBC, 2015; Max and Johnson, 2016).

Water (host molecules) and molecules of gases or liquids (guest molecules) form ice-like structures together at high pressure and low temperature conditions (Sloan and Koh, 2008; Liu, 2013). These ice-like structures are called “gas hydrates” if the guest molecules are in gaseous state (Carroll, 2009). Approximately 130 compounds form hydrates (Sloan and Koh, 2008). Methane (CH<sub>4</sub>), ethane (C<sub>2</sub>H<sub>6</sub>), propane (C<sub>3</sub>H<sub>8</sub>), carbon dioxide (CO<sub>2</sub>), nitrogen (N<sub>2</sub>), hydrogen sulfide (H<sub>2</sub>S), etc. can create their own gas hydrates or mixed hydrates when appropriate pressure and temperature conditions are met (Giavarini and Hester, 2011). Depending on the molecular diameter of hydrate former

(guest molecule), different gas hydrate structures form: mainly structure I (sI) and structure II (sII). Structure H (sH) rarely exists in nature. Different types of cages compose each gas hydrate structure. These cages are pentagonal dodecahedron (5<sup>12</sup>), tetrakaidecahedron (5<sup>12</sup>6<sup>2</sup>), hexakaidecahedron (5<sup>12</sup>6<sup>4</sup>), irregular dodecahedron (4<sup>3</sup>5<sup>6</sup>6<sup>3</sup>) and icosahedron (5<sup>12</sup>6<sup>8</sup>). For example, pentagonal dodecahedron (n<sup>m</sup> = 5<sup>12</sup>) is formed from 12 (m = 12) pentagonal (n = 5) faces. Hence, n and m numbers are used to define the shape of different cages of hydrates. One sI hydrate structure consists of 2 pentagonal dodecahedron cages (small cages: 5<sup>12</sup>) and 6 tetrakaidecahedron cages (large cages: 5<sup>12</sup>6<sup>2</sup>). sII hydrate structure is larger than sI hydrate structure and they are composed of 16 small cages (5<sup>12</sup>) and 8 large cages (hexakaidecahedron: 5<sup>12</sup>6<sup>4</sup>). Finally, sH hydrate consists of 3 small (5<sup>12</sup>), 2 mediums (4<sup>3</sup>5<sup>6</sup>6<sup>3</sup>) and 1 large cages (5<sup>12</sup>6<sup>8</sup>) (Sloan, 2003; Zou, 2013). Approximately 46, 136 and 34 water (H<sub>2</sub>O) molecules are essential for sI, sII and sH hydrates, respectively. CH<sub>4</sub>, C<sub>2</sub>H<sub>6</sub>, CO<sub>2</sub>, and H<sub>2</sub>S establish sI hydrates and C<sub>3</sub>H<sub>8</sub> and N<sub>2</sub> form sII hydrates (Sloan and Koh, 2008). In nature, approximately, 99% of gas hydrates is CH<sub>4</sub> hydrate (Kvenvolden, 1995; Max et al., 2013). Moreover, at least 95% of gas hydrates in nature are found in marine environment while the rest are found in permafrost regions (Max and Johnson, 2016).

There is a controversy about the amount of CH<sub>4</sub> hydrate in the

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world but it is thought that even the most conservative estimates of the total quantity of CH<sub>4</sub> in CH<sub>4</sub> hydrates are much larger than the conventional gas resources (404 tcm) and shale gas (204 tcm–456 tcm) (Johnson, 2011; Chong et al., 2016). The magnitude of this resource can make hydrate reservoirs a substantial future energy resource. Gas production from the coarse sands saturated with gas hydrates might be feasible with current technology because porosity and permeability are high in coarse sands (Boswell, 2014; Max and Johnson, 2016; Heeschen et al., 2016; Boswell et al., 2017).

Currently, there are mainly four production methods from gas hydrate reservoirs: depressurization, thermal injection, chemical injection and CH<sub>4</sub>-CO<sub>2</sub> replacement (Moridis et al., 2013; Xu and Li, 2015; Chong et al., 2016). Depressurization method is applied by reducing reservoir pressure below hydrate equilibrium pressure. It is considered that this method is the most economically viable method because no external energy is used. However, its disadvantages include a slow rate of production and the risk of reservoir subsidence (Konno et al., 2010; Huang et al., 2016). In thermal injection, mainly external heat is introduced to gas hydrate reservoirs by injecting hot water, steam or microwaves so gas hydrate equilibrium is disturbed (Liang et al., 2008; Xu and Li, 2015). The disadvantages of this method are low injection rate and low energy efficiency. Hence, for different gas hydrate reservoirs, it is suggested to combine this method with depressurization method or chemical injection method for feasible gas production (Yuan et al., 2013; Feng et al., 2015; Minagawa et al., 2015). Among four gas hydrate production methods, chemical injection method is the least preferred approach. Although chemical injection shifts gas hydrate equilibrium curve to higher pressures and lower temperatures for gas hydrate dissociation, its disadvantages are low injection rate (mostly due to low effective permeability of gas hydrates), low-cost efficiency and environmentally harmful (Moridis et al., 2013; Chong et al., 2016; Max and Johnson, 2016). CH<sub>4</sub>-CO<sub>2</sub> replacement or CO<sub>2</sub> injection method is quite different from depressurization method, thermal injection method and chemical injection method (Ohgaki et al., 1996). Below 283.2 K, CO<sub>2</sub> hydrate is much more stable than CH<sub>4</sub> hydrate as shown in Fig. 1 (Goel, 2006). When CO<sub>2</sub> is injected into CH<sub>4</sub> hydrate reservoirs, CH<sub>4</sub> molecules leave their hydrate cages and CO<sub>2</sub> molecules fill these empty cages due to the difference in chemical potentials of both systems. CO<sub>2</sub> has high chemical potential in gas phase and zero in gas hydrate but CH<sub>4</sub> shows the opposite. This difference and initially very steep gradients drive the replacement (Xu and Li, 2015). CH<sub>4</sub>-CO<sub>2</sub> replacement method in gas hydrates is advantageous due to CO<sub>2</sub> sequestration, low water production and low geomechanical risks (Hyodo et al., 2014).

Table 1 summarizes the advantages and disadvantages of CH<sub>4</sub>-CO<sub>2</sub> replacement. The recovery of CH<sub>4</sub> might be up to 64% with CO<sub>2</sub> injection to CH<sub>4</sub> hydrates (Nago and Nieto, 2011). CH<sub>4</sub> hydrate and CO<sub>2</sub>

**Table 1**

Advantages and disadvantages of CH<sub>4</sub>-CO<sub>2</sub> replacement (Geng et al., 2009; Zhao et al., 2012; Hyodo et al., 2014; Abbasov et al., 2016; Liu et al., 2016).

Advantages	Disadvantages
A good alternative for CO <sub>2</sub> sequestration and gas production method	Operational difficulties for CO <sub>2</sub> injection (CO <sub>2</sub> hydrate formation) and extra cost of CO <sub>2</sub> injection
Less geomechanical risks in sediments	Slow injection rate due to low effective permeability of gas hydrates and slow replacement rate
Less water production	Low recovery of CH <sub>4</sub>

hydrate are sI type of gas hydrates (2 large cages and 6 small cages). The ratio of molecular diameter of CO<sub>2</sub> to cavity diameter of sI hydrate structure is 1.0 for small cages and 0.834 for large cages but CH<sub>4</sub> easily fills both small and large cages of sI hydrate (Sloan and Koh, 2008). Consequently, CH<sub>4</sub>-CO<sub>2</sub> replacement is extremely low in small cages and mostly CH<sub>4</sub> molecules stay in the small cages of sI hydrate (Yuan et al., 2012). Furthermore, the content of small cages remains largely immobile due to very low probability of a molecule from small cage to jump into the large cage and then reach the gas hydrate surface. The exchange has its preferred paths namely interconnected large cages. Small cages are just sinks or dead ends. After the production of approximately 64% of CH<sub>4</sub> from CH<sub>4</sub> hydrate via CO<sub>2</sub> injection, the mixed CH<sub>4</sub>-CO<sub>2</sub> hydrate in the sediments keep the sediments geomechanically much more stable compared to other production methods (Geng et al., 2009; Hyodo et al., 2014; Liu et al., 2016). This study reviews the application of CH<sub>4</sub>-CO<sub>2</sub> replacement method, the first field tests of CH<sub>4</sub>-CO<sub>2</sub> replacement in Ignik Sikumi field in 2012, laboratory studies in micro scale and pore network modelling studies. However, it is also essential to review some macro-model studies and their deficits to indicate why micro-scale and pore network modelling studies are needful.

## 2. Field study of CH<sub>4</sub>-CO<sub>2</sub> replacement

The injection of CO<sub>2</sub> through gas hydrate reservoirs is generally a major problem because of low permeability. When high CO<sub>2</sub> injection pressures are observed in impermeable or low permeable gas-hydrate bearing sediments, CO<sub>2</sub> phase changes easily from gaseous state to liquid or supercritical state (Goel, 2006). High CO<sub>2</sub> injection pressure increases the possibility of formation of pure CO<sub>2</sub> hydrate when there is free water in the pores. As pure CO<sub>2</sub> hydrate is constituted instead of the CH<sub>4</sub>-CO<sub>2</sub> hydrate replacement, the permeability of hydrate reservoir decreases further. In order to increase the effectiveness of CO<sub>2</sub> injection and to avoid the CO<sub>2</sub> injection problem at high pressures, 77% N<sub>2</sub> and 23% CO<sub>2</sub> mixture injection to CH<sub>4</sub> hydrates was suggested by University of Bergen and it was proved experimentally and also in Ignik Sikumi field pilot project (Schoderbek et al., 2013; Kvamme, 2015, 2016). During replacement processes in experimental studies, it was observed that large cages of sI hydrate filled by mostly CO<sub>2</sub> and small cages are filled by N<sub>2</sub>. Thus, CH<sub>4</sub> recovery was increased from 64% to 85% by injecting the mixture of CO<sub>2</sub> and N<sub>2</sub>. This also avoids the injection problem of CO<sub>2</sub> and reduces the chance of pure CO<sub>2</sub> hydrate formation because N<sub>2</sub> concentration is high. Moreover, N<sub>2</sub> can only create its pure sII hydrate at very high pressure (i.e. ~8.94 MPa at 281.15 K) (Sloan and Koh, 2008; Carroll, 2009). It also increases the recovery of CH<sub>4</sub> by replacing CH<sub>4</sub> in small cages with injected N<sub>2</sub>. In another studies of Kang et al. (2014) and Ahn et al. (2015), air and CO<sub>2</sub> injection (flue gas) was suggested for gas production from CH<sub>4</sub> hydrates with the replacement mechanism because it is feasible to obtain flue gas rather than preparing CO<sub>2</sub>/N<sub>2</sub> gas mixture. The efficiency of CH<sub>4</sub>-CO<sub>2</sub> (20%)/air (80%) replacement in the study of Kang et al. (2014) and Ahn et al. (2015) exceeded approximately 85%.

Different from the previous pilot projects (i.e. depressurization tests) on gas hydrate reservoirs, CO<sub>2</sub>/N<sub>2</sub> mixture was injected into the

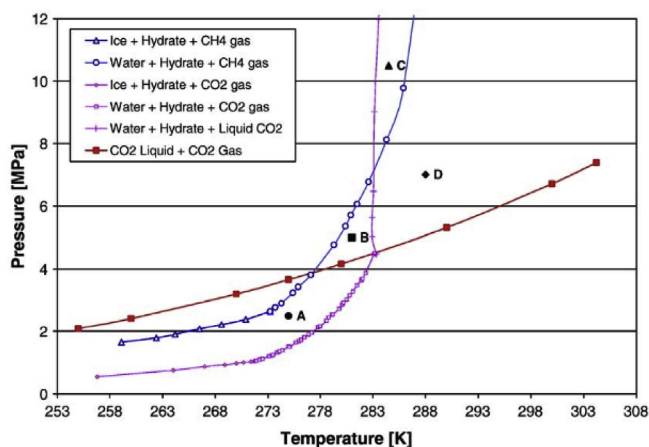


Fig. 1. Hydrate equilibrium curves of CH<sub>4</sub> and CO<sub>2</sub> (Goel, 2006).

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