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# Use of low- and high-IFT fluid systems in experimental and numerical modelling of systems that mimic CO<sub>2</sub> storage in deep saline formations



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#### ABSTRACT

Storage of  $CO_2$  in deep saline formations is currently the most promising option for mitigating the impact of climatic changes. Therefore, it is important to understand flow processes and distribution of forces acting on injected CO<sub>2</sub>. To demonstrate the influence of gravitational, viscous, and capillary forces on the flow of CO<sub>2</sub>, special experiments were designed. Laboratory experiments and numerical simulations were performed, where fluid representing CO<sub>2</sub> was injected into a 2D porous medium saturated with fluid representing brine. Two sets of fluids characterised by different interfacial tension (IFT) were tested. Results demonstrate that at increasing injection rate viscous forces become stronger, leading to a higher total displacement of brine. Such performance is preferred at field scale, since it facilitates dissolution and residual trapping of CO<sub>2</sub>. Gravity effects were more pronounced in cases with low injection rates and high permeability and are demonstrated by lower volumes of the in-situ fluid displacement. Therefore, reservoirs giving low influence of gravity forces are more suitable for CO<sub>2</sub> storage. The high-IFT fluid system had an IFT corresponding to the value of CO<sub>2</sub>-brine systems at possible reservoir conditions. However, the fluid flow in the laboratory model was dominated by capillary forces. This kind of behaviour is less likely to be observed at field scale as it is a result of the much smaller volume of porous system used in the laboratory compared to the volume at the field scale. The low-IFT fluid system resembled better field scale flow behaviour. The laboratory experiments were also modelled using a numerical reservoir simulation software. While modelling of observations from high-IFT system was challenging, simulations for low-IFT displacements showed accurate reflection of experiments.

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#### 1. Introduction

Since the late 19th century, the Earth's surface temperature has increased and the evidence on climate change has grown substantially (Stocker et al., 2013). The main cause of climate change is attributed to deforestation and increase in anthropogenic emissions of  $CO_2$  and other greenhouse gases in the atmosphere originating from fossil fuel combustion. Since the start of the industrial revolution in the mid-18th century mankind has produced approximately 337 billion metric tonnes of  $CO_2$  and half of this amount has been emitted since the mid-1970s (Boden et al., 2010). Currently  $CO_2$  emissions from fossil fuels are approximately 8.4 billion metric tonnes (Gtonnes) per year (Boden et al., 2010). As

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http://dx.doi.org/10.1016/j.petrol.2015.02.031 0920-4105/© 2015 Elsevier B.V. All rights reserved. the emissions of  $CO_2$  are predicted to increase in the future (IPCC, 2007) it is important to find efficient methods of limiting its release to the atmosphere.

Storage of  $CO_2$  in deep geological formations is one of the measures for mitigating the impact of climatic changes (IPCC, 2005). Currently the most promising option for geological  $CO_2$  storage is thought to be deep saline formations, due to their large, immediately available capacity (IPCC, 2005). Saline formations are sedimentary rock saturated with brine which is not suitable either for human consumption or for agriculture (e.g. IPCC, 2005). Global storage capacity in saline aquifers was estimated to be in the range of 1000–10,000 Gtonnes (IPCC, 2005; IEA-GHG, 2008). This could mean that all  $CO_2$  produced in this century (assuming current yearly levels) could be stored underground if the capacity of the saline aquifers would be efficiently used and storage sites would prove to be safe.

Nomenclature	N <sub>C</sub> capillary number
	P pressure, bar
<i>A</i> cross-section surface area, m <sup>2</sup>	<i>P</i> <sub>c</sub> capillary pressure, bar
<i>a</i> , <i>b</i> , <i>c</i> , <i>d</i> empirical constants in relative permeability	PV pore volume fraction
calculations	$\phi$ porosity
$d_b$ glass-bead diameter, m or $\mu$ m	<i>q</i> flow rate, m <sup>3</sup> /s
$\Delta p$ pressure drop, Pa	<i>R</i> <sub>CG</sub> capillary to gravity forces ratio
$\Delta \rho$ density difference of the fluids, kg/m <sup>3</sup>	<i>R</i> <sub>VG</sub> viscous to gravity forces ratio
g acceleration of gravity, m/s <sup>2</sup>	$\rho_{\rm nw}$ density of non-wetting phase, kg/m <sup>3</sup>
γ interfacial tension, IFT, mN/m	$\rho_{\rm w}$ density of wetting phase, kg/m <sup>3</sup>
<i>h</i> distance between model's inlet and top outlet, m	<i>S</i> <sub>nwr</sub> non-wetting phase residual saturation
<i>k</i> permeability, m <sup>2</sup> or mD or D	S <sub>w</sub> wetting phase saturation
<i>k</i> <sub>rnw</sub> non-wetting phase relative permeability	<i>S</i> <sup>*</sup> <sub>w</sub> effective wetting phase saturation
<i>k</i> <sub>rw</sub> wetting phase relative permeability	<i>S</i> <sub>wi</sub> wetting phase irreducible saturation
L glass-bead pack length, m	<i>u</i> Darcy's flow velocity, m/s
$\mu$ fluid viscosity, Pa s	

Every potential geological storage site considered for use in carbon capture and storage (CCS) must be carefully investigated and the flow processes taking place within such reservoirs must be understood. The characteristics of flows that occur when  $CO_2$  is injected into a deep geological formation control how much  $CO_2$  can be effectively injected and stored within the formation. Understanding of processes that take place within a saline formation during and after  $CO_2$  injection is essential in order to select a suitable storage site. Flow regimes that occur when  $CO_2$  is injected into a geological formation control how much  $CO_2$  can be stored in the formation. Therefore, selection of a geological storage site for  $CO_2$  must be preceded by an accurate understanding of the flow processes that take place within the reservoir during and after injection.

In recent years numerous analytical and numerical studies have been undertaken that concern site characterisation for  $CO_2$  injection/ storage and describe the simultaneous flow of  $CO_2$  and brine in subsurface formations (e.g. Nordbotten et al., 2005; Taku Ide et al., 2007; Wood et al., 2008; Kopp et al., 2009). However, experimental data that shed light on the nature of the drainage process which applies to  $CO_2$  injection has been less frequently reported. Fluid flow in the parameter range appropriate for  $CO_2$  storage in saline aquifers has been studied in both 2D (Hele-Shaw-like) and cylindrical models filled with glass-beads (e.g. Cinar et al., 2009; Islam et al., 2013). In addition, pore-scale micro-models (e.g. Chapman et al., 2013), sandpacks (e.g. Pentland et al., 2010; Al Mansoori et al., 2010) and consolidated rocks (e.g. Berg et al., 2013) were used to study various aspects of fluid behaviour in the porous media with respect to  $CO_2$ storage.

Systems with immiscible fluids, characterised by high interfacial tension (IFT), were commonly used in order to model flow patterns under  $CO_2$  injection. Such experimental set-up provides information on the behaviour of fluid displacement in addition to the data which can be used in numerical simulations. Furthermore, experimental procedures can be successfully employed in order to verify results of analytical and numerical studies. The main advantage of these experiments is the possibility to visually assess the behaviour of the fluids in the model.

 $CO_2$  and brine are immiscible at reservoir conditions and they form a high-IFT fluid system where  $CO_2$ -brine IFT falls between 20 and 56 mN/m (Bennion and Bachu, 2006; Chiquet et al., 2007). Therefore, the high-IFT system is usually a first choice when one tries to mimic  $CO_2$  and brine interaction. Past work on fluid flow in high-IFT systems often demonstrated by the means of Hele-Shaw cell (e.g. Saffman and Taylor, 1958; Homsy, 1987; Løvoll et al., 2005; Duan and Wojtanowicz, 2007) indicates that the most visible feature is the pronounced fingering of injected fluid which dominates the flow. At lower IFT, however, it is possible to observe a more stable and uniform displacement front in addition to finer, viscous fingering. Further, as demonstrated previously (Cinar et al., 2006; Asghari and Torabi, 2008; Islam et al., 2013), it is problematic to simulate accurately laboratory-scale high-IFT experiments in commercial fluid flow simulators. Nevertheless, in this work, we present an approach for simulating a high-IFT system that resembles the effects observed in the experiments. In addition to the high-IFT system, a low-IFT system was investigated in order to observe the finer details of fluid flow behaviour on a smaller scale. Furthermore, it has been demonstrated that the low-IFT system is more suitable for simulations at the laboratory scale.

Additionally, the paper presents findings obtained during experimental examination of the flow processes that normally take place within a saline formation during  $CO_2$  injection. In the procedures,  $CO_2$ is represented by a model fluid injected into a model system of saline aquifer. Influence of low- and high-IFT fluid systems on the flow patterns is demonstrated along with results of the numerical simulations from modelling of the laboratory experiments.

#### 2. Material and methods

Quasi two-dimensional experiments were performed in a synthetic porous medium initially filled with a water-rich phase. The model was made of two vertical glass plates with space between them packed with glass-beads. Models used in the experiments represented homogeneous porous media where the glass-bead size controlled their permeability. Two sets of fluids with different IFT were used in the experiments.

In the field applications,  $CO_2$  is normally injected at the bottom of the geological formation. Even in a supercritical state, it is less dense than in-situ brine, and it tends to migrate up, towards the top of formation. In such a case, gravity forces will cause instabilities in the displacement front. Additionally, high viscosity difference between fluids at the reservoir conditions indicates the instability caused by the viscosity difference. Therefore gravity and viscous unstable floods were most suitable to experimentally model  $CO_2$  injection into brine-filled formations. Experiments were designed in a way that demonstrate the influence of gravitational, viscous and capillary forces on the vertical flow of  $CO_2$ . Further, experiments were modelled by means of ECLIPSE 100, a commercial numerical reservoir simulation software. Download English Version:

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