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# In-line mixing states monitoring of suspensions using ultrasonic reflection technique

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## ABSTRACT

Based on the measurement of echo signal changes caused by different concentration distributions in the mixing process, a simple ultrasonic reflection technique is proposed for in-line monitoring of the mixing states of suspensions in an agitated tank in this study. The relation between the echo signals and the concentration of suspensions is studied, and the mixing process of suspensions is tracked by in-line measurement of ultrasonic echo signals using two ultrasonic sensors. Through the analysis of echo signals over time, the mixing states of suspensions are obtained, and the homogeneity of suspensions is quantified. With the proposed technique, the effects of impeller diameter and agitation speed on the mixing process are studied, and the optimal agitation speed and the minimum mixing time to achieve the maximum homogeneity are acquired under different operating conditions and design parameters. The proposed technique is stable and feasible and shows great potential for in-line monitoring of mixing states of suspensions.

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## 1. Introduction

Mixing is a fundamental and important process which has a wide range of applications in the fields like fine chemicals, mineral processing and polymer processing [1]. The mixing states have significant effects on products [2]. For example, the mixing state of solid propellant slurry directly affects its mechanical properties and combustion characteristics [3]. The mixing states of suspensions depend on the operating conditions (e.g. the agitation speed and the mixing time), the design parameters (such as the impeller diameter) and so on [4]. In general, the higher the agitation speed is and the longer the mixing time is, the better the homogeneity of suspensions is. However, once the suspensions reach the maximum achievable homogeneity, it will be useless for the improvement of suspensions performance and even inevitably raise the cost of production to further increase the impeller speed and/or prolong the mixing time. At the same time, it is not easy to judge whether these parameters are appropriate. Therefore, the studies on the mixing states of suspensions will provide the researchers an access to the optimal operating conditions and design parameters.

So far, several methods have been proposed to study the mixing states of suspensions. The investigation of particle suspension characteristics with conductivity probes is accurate but intrusive, and subject to the flow disturbance to a certain extent [5]. Visual methods are commonly used to determine the mixing states of suspensions through observing the particle remaining time [6], the cloud height [7] or the settled bed height [8]. Optical methods can be used to measure the solid concentration profiles through measuring the light intensity attenuation [9] or the multiple light scattering [10]. Despite the advantage that visual methods and optical methods have no disturbance to the flow patterns, it is necessary to fabricate transparent agitated tanks in order to observe the mixing states of suspensions. The fabrication of transparent agitated tanks can be easily realized at the laboratory scale but is impractical for large-scale industrial applications. The pressure gauge method [11] is very suitable to measure the fraction of suspended solids in the industrial application, but this method is likely to be affected by the flow patterns. Recently, the industrial process tomography (IPT) techniques, e.g., electrical resistance tomography (ERT) [12], electrical impedance tomography (EIT) [13] and magnetic resonance imaging (MRI) [14], are developed to study the mixing states of suspensions. Nevertheless, IPT techniques are generally confronted with the problems of high cost and complexity.

Owing to the advantages of stability and cost-effectiveness [15], ultrasonic sensors can provide real-time measurement of the

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87 mixing states of suspensions with high temporal and spatial resolu-  
 88 tion [16]. The ultrasonic techniques have been extensively  
 89 applied in the process industry [17,18]. Stelzer et al. [19] adopted  
 90 the ultrasonic crystallization monitoring technique to quantify  
 91 the industrial crystallization process. Hunter et al. [20] studied  
 92 the settling and sedimentation processes in particle dispersion  
 93 with the ultrasonic velocimetry technique. A wealth of literature  
 94 is available on the application of ultrasonic methods for the mea-  
 95 surement of the suspensions properties (e.g. density [21], concen-  
 96 tration [22] and particle size [23]). However, the studies regard-  
 97 ing of the mixing process of suspensions are still limited. Bamberger  
 98 and Greenwood [24] put forward a simple single frequency ultra-  
 99 sonic technique to in-line measure the ultrasonic attenuation and  
 100 track the slurry mixing process, but ultrasonic sensors were com-  
 101 pletely immersed in suspensions, which exerted certain effects  
 102 on the mixing flow field. Yucel and Coupland [25] mounted a single  
 103 transmitter–receiver pair in the agitated tank to measure the mix-  
 104 ing, agglomeration and quiescent sedimentation of sucrose crystals  
 105 in vegetable oil. This study gave a good indication for the kinetics  
 106 and extent of the mixing process of suspensions and described the  
 107 steady mixing state. Nevertheless, the mixing states of suspensions  
 108 and the relations among the mixing states, mixing time, homo-  
 109 geneity and mixing parameters of suspensions need further  
 110 studies and the ultrasonic techniques should be further improved  
 111 to better meet the requirements of monitoring the mixing states  
 112 of suspensions.

113 In this study, a simple ultrasonic reflection technique is pro-  
 114 posed and the mixing process and states of small particle suspen-  
 115 sions (the non-dimensional wave number  $kr \ll 1$  [23]) with  
 116 moderate volume concentration in an agitated tank are monitored  
 117 using two ultrasonic sensors. The criteria to determine the states of  
 118 suspensions are presented and the homogeneity of suspensions is  
 119 quantified. The effects of the impeller diameter and the agitation

120 speed on the mixing process are studied. The optimal agitation  
 121 speed and the minimum mixing time to achieve the maximum  
 122 homogeneity under different testing conditions are also discussed.  
 123 The proposed technique can find facile and inexpensive applica-  
 124 tions in both laboratories and the industrial field.

125 **2. Materials and methods**

126 *2.1. Experimental setup*

127 The experimental setup is shown in Fig. 1(a). The mixing system  
 128 consisted of a transparent flat-bottomed cylindrical tank, with an  
 129 inner diameter ( $T$ ) of 130 mm and a height ( $h$ ) of 150 mm, respec-  
 130 tively. To avoid dead zones as well as vortexes, four standard baf-  
 131 fles, with the width ( $B$ ) of  $T/12$ , were symmetrically fixed to the  
 132 inner wall of agitated tank [4]. Both the agitated tank and the baf-  
 133 fles were made of polymethyl methacrylate (PMMA). The agitation  
 134 speed was adjusted with an adjustable-speed motor. The mixing  
 135 system was agitated using four-bladed 45° pitched blade turbine  
 136 (PBT-4) impellers and the impeller diameters ( $D$ ) were 50 mm,  
 137 60 mm and 70 mm, respectively. The clearance ( $C$ ) between the  
 138 impeller and the bottom of agitated tank was one fourth of the  
 139 height of suspensions ( $H$ ).

140 The ultrasonic system was composed of two Olympus V306-SU  
 141 ultrasonic immersion sensors (with a center frequency of  
 142 2.25 MHz) and two ultrasonic Pulser/Receiver units in the pulse-  
 143 echo mode. One end of the buffer rod was bonded to the ultrasonic  
 144 sensor TRA, while the other end was slightly submerged into the  
 145 suspensions and positioned parallel to the bottom of the agitated  
 146 tank which acted as a reflector plate. The buffer rod was made of  
 147 PMMA as well. The ultrasonic sensor TRB was bonded to the bot-  
 148 tom of the agitated tank using couplant. The two sensors were  
 149 mounted close to the wall of agitated tank and separated by the

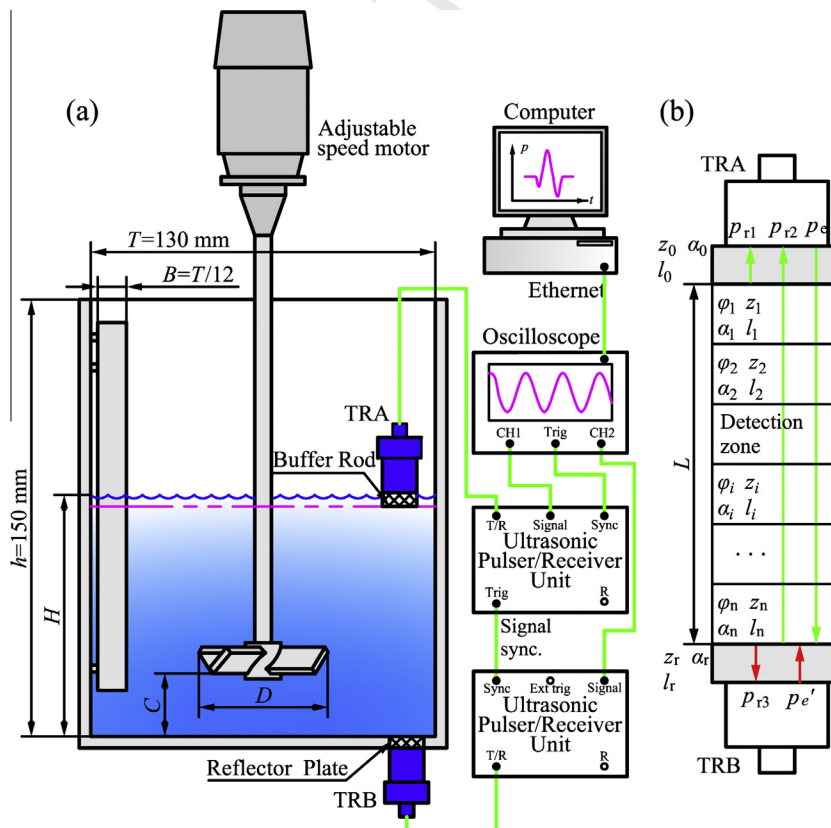


Fig. 1. (a) The experimental setup. (b) The schematic measuring principle.

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