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## Spectroscopic study on transformations of Q3 dissolved organic matter in coal-to-liquids

- 2 wastewater under integrated chemical oxidation
- 3
- and biological treatment process 4

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## ABSTRACT

A large amount of wastewater containing various toxic organic contaminants is produced 17 Q6 during coal pyrolysis. In this study, several spectroscopic methods were used to monitor 18 the transformation of organic pollutants during an integrated chemical oxidation and 19 biological process. The results showed that the hydrophobic acid fraction increased after 20 Fenton oxidation, which was likely due to the production of small-molecule organic acids. 21 Soluble microbial products were generated during biological treatment processes, which 22 were degraded after ozonation; meanwhile, the hydrophilic base and acid components 23 increased. Ultraviolet-visible spectroscopic analysis indicated that peaks at the absorption 24 wavelengths of 280 and 254 nm, which are associated with aromatic substances, were 25 detected in the raw water. The aromatic substances were gradually removed, becoming 26 undetectable after biological aeration filter (BAF) treatment. Fourier transform infrared 27 spectroscopy analysis revealed that the functional groups of phenols; benzene, toluene, 28 ethylbenzene, and xylene (BTEX); aromatic hydrocarbons; aliphatic acids; aldehydes; and 29 esters were present in raw wastewater. The organic substances were oxidized into small 30 molecules after Fenton treatment. Aromatic hydrocarbons were effectively removed through 31 bioadsorption and biodegradation after BAF process. Biodegradable organic matter was 32 reduced and finally became undetectable after anoxic-oxic treatment in combination with 33 a membrane bioreactor. Four fluorescent components were fractionated and obtained via 34 excitation-emission matrix parallel factor analysis (EEM-PARAFAC). Dissolved organic matter 35 fractionation in conjunction with EEM-PARAFAC was able to monitor more precisely the 36 evolution of characteristic organic contaminants. It was concluded that the integrated 37 treatment process was effective in removing the characteristic organic contaminants in coal- 38 to-liquids wastewater.

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## ARTICLE IN PRESS

### 55 Introduction

56 With the gradual consumption of petroleum resources, much attention has been paid to the coal liquefaction industry 57 Q8 Q7 worldwide (Huang and Yuan, 2015; Wei and Shi, 2015). Coalto-liquid (CTL) is a strategic industry for replacing petroleum 59 resources, and thus a measure that can safeguard Chinese 60 61 energy security. Beyond that, the coal liquefaction industry is 62 not only important for realizing clean and efficient utilization 63 of coal, but also is necessary for improving the quality of fuel 64 oil. Optimization of the production technology of coal-to-oil 65 can promote the transformation and upgrading of the coal industry and help solve the problems regarding coal produc-66 67 tion capacity and related issues.

The rapid development of the CTL industry in China has 68 brought extensive attention to the treatment of effluent 69 70 produced via coal liquefaction. CTL processes generate a large amount of wastewater, which characteristically has a high 71 organic concentration and low biodegradability. The chemical 72 73 oxygen demand (COD) of this wastewater is generally around 9000–10,000 mg/L. In addition, CTL wastewater is very complex 74 75 in its chemical composition of organic matter and contains 76 many toxic and bioresistant organic substances, such as hydrocarbons, aldehydes, phenols, and benzenes. 77

78 The characteristics of the dissolved organic matter (DOM) 79 in wastewater affect the treatability and process options for 80 the wastewater (Jiang et al., 2017). Because of the complex constituents of DOM in CTL wastewater, traditional biological 81 82 processes alone are unable to purify wastewater effectively, 83 so combined physicochemical and biological processes are always used for such wastewater (Yue et al., 2015; Sahu et al., 84 2017). Actually, integrated processes have been established 85 and operated for many years in China for CTL wastewater 86 treatment. In particular, desulfurization, dephenolization, 87 and deamination pretreatments are conducted first for 88 separation of sulfide ions, phenols, and ammonium, respec-89 tively (Hou et al., 2014; C.Q. Han et al., 2010; H.J. Han et al., 90 91 2010). After that, Fenton oxidization is used to detoxify the wastewater and improve its biodegradability (Peng et al., 92 2016), and then the wastewater is treated further via an 93 efficient biological aeration filter (BAF). To remove the 94 residual organic matter in the wastewater, an integrated 95 ozonation preoxidation and anoxic-oxic (A/O) process is 96 applied (Nawrocki and Kasprzyk-Hordern, 2010; Barker and **Q**9 Q10 Stuckey, 1999; Deng et al., 2017). Finally, the A/O effluent is treated in depth by a membrane bioreactor (MBR) for water 99 reclamation. 100

At present, most of the CTL wastewater in China conforms 101 to the emission standard after such treatment, but the 102 effluent might contain some toxic substances at trace 103 concentrations. Few studies have focused on the monitoring 104 and evaluation of these trace toxic organic pollutants in CTL 105 106 wastewater treatment (Lu et al., 2006), yet most of these 107 substances have carcinogenic, teratogenic, and mutagenic effects and pose a great threat to ecological security and 108 human health. In addition, it has been difficult to observe the 109 changes undergone by organic pollutants during the actual 110 treatment of CTL wastewater. Therefore, it was necessary to find 111 a simple and effective method to monitor the characterization 112

of the changes in organic pollutants during CTL wastewater 113 treatment processes. 114

Spectroscopic methods have been widely used for charac- 115 terization of dissolved organic contaminants in wastewaters 116 from different industrial sources. Li et al. (2017) investigated 117 the migration and transformation of organic compounds in 118 wastewater from physicochemical treatment processes by 119 using different spectroscopic methods. They applied ultravi- 120 olet absorbance (UVA) and fluorescence techniques to assess 121 the formation of biodegradable dissolved organic carbon 122 (BDOC) and bromate during ozonation and suggested that 123 measurement of UVA was able to assess the formation of 124 BDOC and bromate. They employed LED ultraviolet (UV) 125 fluorescence sensors to monitor DOM online to predict the 126 formation potential of disinfection by-products (DBPs) during 127 water disinfection treatment. It was found that both protein- 128 like and humic-like fluorescence can be excited by UV280 129 LED and then detected via photodiodes combined with light 130 filters  $(350 \pm 15 \text{ nm and } 440 \pm 30 \text{ nm}, \text{ respectively})$  and that 131 the UVA at 280 nm can substitute for the UVA at 254 nm for 132 online monitoring of DOM and for predicting DBP formation 133 potential (Li et al., 2016). Fluorescence analysis combined 134 with parallel factor analysis (PARAFAC) is widely used to 135 predict the transformation of typical DOM in water treatment 136 processes or in aquatic environments. Li studied the changes 137 in DOM during municipal wastewater treatment using fluo- 138 rescence analysis and PARAFAC (Li et al., 2014). In addition, 139 Osburn et al. (2012) combined excitation-emission matrix 140 (EEM) fluorescence and PARAFAC analysis to model base- 141 extracted particulate organic matter (POM) and DOM compo- 142 sitions in the Neuse River Estuary (NRE). It was demonstrated 143 that four PARAFAC components (C1-C3 and C6) were derived 144 from terrestrial sources to the NRE, one component (C4) 145 was enriched in the POM and in surface sediment pore water 146 DOM, and one component (C5) was related to recent autoch- 147 thonous production. Sgroi et al. (2017) used EEM and different 148 data processing methods, including peak-picking methods, 149 Fourier transform infrared (FT-IR) analysis, and PARAFAC, to 150 evaluate their suitability for producing effective surrogate 151 pollutant indices. Use of a convenient and sensitive fluores- 152 cence analytical technique as a monitoring tool could quickly 153 reveal the removal and conversion of organic compounds in 154 different water bodies. 155

As mentioned above, CTL wastewater contains different 156 kinds of harmful organic contaminants, but few studies 157 have focused on the transformation of these pollutants at 158 the molecular level throughout the wastewater treatment 159 process. In this study, we combined the methods of UV 160 spectroscopy, FT-IR spectroscopy, and EEM fluorescence 161 spectroscopy to systematically investigate the molecular 162 structure and transformation of organic components during 163 an integrated treatment process for CTL wastewater. In addi- 164 tion, gas chromatography-mass spectrometry (GC-MS) was 165 conducted to analyze the variation of organic matter in CTL 166 wastewater and verify the accuracy of the spectroscopic 167 analysis (Appendix A Fig. S9 and Table S1). The objective of 168 this study was to gain insight into the transformation mecha- 169 nisms of organic pollutants in different wastewater treatment 170 stages and to evaluate the operating efficiency of the integrated 171 process for CTL wastewater treatment. 172

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