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# 1 Anaerobic treatment of source-separated domestic bio-wastes 2 with an improved upflow solid reactor at a short HRT

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## A B S T R A C T

Anaerobic treatment is the core technology for resource and energy recovery from 16  
 source-separated domestic bio-wastes. The higher efficiency of an improved upflow solid 17  
 reactor (IUSR) designed in this study was demonstrated in the treatment of concentrated 18  
 black water and kitchen waste. The highest methane production of 48 L/person/day was 19  
 achieved at the hydraulic retention time (HRT) of 7 days, while the other measures of 20  
 performance at the HRT of 8.3 days were better than at the HRT of 7 or 10 days, achieving a 21  
 methane production of 43 L/person/day, removal of total chemical oxygen demand (TCOD) 22  
 of 89%, removal of soluble chemical oxygen demand (SCOD) of 92%, and conversion of 23  
 chemical oxygen demand (COD) to methane of 71%. It is not recommended to decrease HRT 24  
 lower than 7 days due to the instability of the initial period. The concentrations of volatile 25  
 fatty acids (VFAs) in the IUSR were less than 10 mg/L, indicating that the anaerobic process 26  
 was stable. Sludge bed development showed that sludge bed with high microbial activity 27  
 was formed in the bottom and that the precipitation zone of effluents formed should 28  
 preferably occupy 30% of the height of the IUSR. The effluents of the IUSR could be used for 29  
 irrigation in agriculture in combination with a settling tank accompanied by disinfection to 30  
 remove solids and pathogens. 31

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## 46 Introduction

47 Anaerobic treatment is one of the most promising treatment  
 48 technologies for building more sustainable sanitation and is  
 49 considered to be the core technology for resource and energy  
 50 recovery from domestic source-separated bio-wastes (Kujawa-  
 51 Roeleveld et al., 2006; Bernstad and la Cour Jansen, 2012; Larsen  
 Q4 et al., 2013), including concentrated black water (CBW), concen-  
 53 trated brown water (BRW) from vacuum toilets, and kitchen  
 54 waste (KW). However, there are only a few publications  
 55 reporting the anaerobic treatment of source-separated domestic  
 56 bio-wastes in various anaerobic reactors, such as the continuous

stirring tank reactor (CSTR) (Wendland et al., 2006; Rajagopal 57  
 et al., 2013), accumulation reactor (AC) (Kujawa-Roeleveld et al., 58  
 2003; Elmitwalli et al., 2006), upflow anaerobic sludge blanket 59  
 (UASB) (de Graaff et al., 2010a, 2010b; de Graaff et al., 2011a, Q5  
 2011b, 2011c) and UASB-septic tank (UASB-ST) (Kujawa- Q6  
 Roeleveld et al., 2005, 2006; Luostarinen et al., 2007). The CSTR 62  
 reactor is a simpler reactor with a mixer rather than a high-rate 63  
 reactor, because there is no retention of high-activity biomass. 64  
 The simplest and largest reactor is the AC reactor, which is 65  
 continuously fed and discharged at once when it reaches the 66  
 required longer retention time. The AC reactor is recommended 67  
 for more concentrated wastes, like livestock manure, brown 68

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69 water and kitchen waste. The UASB is suitable for treating  
70 bio-substrates with lower solid concentrations, and thus is only  
71 applied to treat concentrated black water, requiring a shorter  
72 hydraulic retention time (HRT) and smaller reactor volume. A  
73 gas/solid/liquid separator and influent distributor are indispens-  
74 able for the UASB, resulting in its complicated configuration. The  
75 UASB-ST reactor, combining the features of a UASB and ST, can  
76 be applied to treat bio-substrates with higher solid concentra-  
77 tions (Fan et al., 2017), like CBW, BRW and KW. Above all, it can  
78 be concluded that development of a more efficient and simple  
79 reactor should be a priority.

80 The upflow solid reactor (USR), derived from the UASB, is  
81 a simple configuration reactor without a gas/solid/liquid  
82 separator and an influent distributor. The USR was first  
83 introduced to treat sea kelp (Srivastava et al., 1988), and had a  
84 longer solids and microorganism retention time than the UASB,  
85 leading to better performance. The USR is known for treating  
86 waste with higher total solid (TS) content, e.g., livestock manure  
87 (Zhou and Yang, 1996), maize silage (Mumme et al., 2010) and  
88 wheat straw (Pohl et al., 2012). It has been reported that the  
89 biogas engineering applications of anaerobic digestion reactors  
90 operating in the surrounding counties of Beijing were generally  
91 dominated by USR technology by 2010 (Chen et al., 2012; Zhou  
92 and Zhou, 2013). However, the weaknesses of USR technology  
93 cannot be ignored, such as its low biomass transfer efficiency  
94 and the problem of encrustation (Wang et al., 2009). USR  
95 technology has not been investigated for the practicability of  
96 treating source-separated domestic bio-wastes, so it needs  
97 further study.

98 Considering the characteristics of mixtures of CBW and  
99 KW, and also the applicability of the USR, the project of this  
100 paper is to demonstrate the practicability of an improved  
101 upflow solid reactor (IUSR) to treat CBW and KW from vacuum  
102 toilets and to identify the optimal operation conditions, such  
103 as HRT and chemical oxygen demand (COD) loadings. In

104 particular, the development of the sludge bed in the reactor  
105 was evaluated, and the potential utilization of the effluent  
106 and sludge was discussed.

## 1. Materials and methods

### 1.1. Feedstock and inoculum sludge

107 The CBW was prepared with feces-urine by collecting the  
108 wastes from a dry toilet and adding some urea to make it  
109 identical with the BW collected from vacuum toilets in  
110 Changshu, Jiangsu Province, China the first demonstration  
111 project applying source separation technologies in rural areas.  
112 According to the eating habits of residents in China (Zhang  
113 and Fu, 2010), KW was made from a mixture of 20% cooked  
114 kitchen waste (CKW) and 80% raw kitchen waste (RKW). The  
115 CKW was collected from a restaurant, and RKW was made up  
116 of 50% pre-prandial waste and 30% fruit waste. The mixed KW  
117 was shredded to a size less than 2 mm. Based on the average  
118 of 5 L of CBW and 500 g KW per person per day in China, the  
119 feedstock used in this study was prepared with KW:CBW =  
120 100 g:1 L, and then was stored at -20°C. Characterization of  
121 the CBW, KW and feedstock mixture is given in Tables 1 and 2.  
122 Because of the much greater amount of KW generated per  
123 person per day (500 g/person/day, China; 200 g/person/day,  
124 Germany (Wendland et al., 2006); 150 g/person/day, Singapore  
125 (Rajagopal et al., 2013)), the feedstock in our study had a higher  
126 concentration of total chemical oxygen demand (TCOD), TS and  
127 volatile solids (VS) compared with other research. The NH<sub>3</sub>-N  
128 content in the feedstock mainly originated from urine. Accord-  
129 ing to Speece (Speece, 1983), most elements were at the optimal  
130 concentrations, while it is notable that concentrations of Fe and  
131 Co were less than the optimal concentrations (10 mg/L Fe and  
132 0.02 mg/L Co).

Table 1 – Characteristics of concentrated black water (CBW), kitchen waste (KW), raw kitchen waste (RKW), cooked kitchen waste (CKW) and the feedstock.

Parameter	RKW	CKW	KW	CBW	Feedstock (5 L CBW + 500 g KW)
TS (%)	13.85	22.40	9.55	0.92	2.1
VS (%)	12.82	20.61	8.67	0.80	1.8
TCOD (a/b)	103.2 <sup>a</sup>	304.5 <sup>a</sup>	175.6 <sup>a</sup>	13,960 <sup>b</sup>	28,554 <sup>b</sup>
SCOD (a/b)	45.4 <sup>a</sup>	70 <sup>a</sup>	54.4 <sup>a</sup>	5134 <sup>b</sup>	13,043 <sup>b</sup>
SCOD/TCOD (%)	43.99	22.99	30.98	36.78	45.68
Total nitrogen (a/b)	1.73 <sup>a</sup>	4.43 <sup>a</sup>	2.62 <sup>a</sup>	597.2 <sup>b</sup>	1353.1 <sup>b</sup>
NH <sub>3</sub> -N (a/b)	0.37 <sup>a</sup>	0.07 <sup>a</sup>	0.92 <sup>a</sup>	196.7 <sup>b</sup>	749.5 <sup>b</sup>
TP (mg/L)	-	-	-	-	202.3
Soluble TP (mg/L)	-	-	-	-	163.1
TVFA (g COD/L)	-	-	-	-	1.07
Acetic-acid (g COD/L)	-	-	-	-	0.64
Propionic-acid (g COD/L)	-	-	-	-	0.26
Isobutyric-acid (g COD/L)	-	-	-	-	0.005
Butyric-acid (g COD/L)	-	-	-	-	0.15
Isovaleric-acid (g COD/L)	-	-	-	-	0.009
Valeric-acid (g COD/L)	-	-	-	-	0.007

Abbreviations: TS—total solid, VS—volatile solid, TCOD—total chemical oxygen demand, SCOD—soluble chemical oxygen demand, TN—total nitrogen, TP—total phosphorus, TVFA—total volatile fatty acid.

<sup>a</sup> and <sup>b</sup> are different units, <sup>a</sup> mg/g, <sup>b</sup> mg/L, \* adding urea, - not measured.

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