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# Pre-treatment of pyridine wastewater by new cathodic-anodic-electrolysis packing

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ABSTRACT

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### 42 Introduction

Pyridine, a type of heterocylic compound, is a chemical raw 43material (Zhao et al., 2011). Pyridine has been widely used in 44 cooking, chemical synthesis, pharmaceutical, and pesticide 45 46 industries, and so on (Sun et al., 2011; Wen et al., 2013). 47 Compared with other aromatic hydrocarbons, pyridine is 48 more difficult to degrade (Li et al., 2016). As a refractory 49organic nitrogen heterocyclic compound, pyridine's deriva-50tives mainly include alkyl pyridines, halogenated pyridines and amino-pyridines, which have been widely used as 51industrial solvents, agriculture herbicides and pesticides 52(Shen et al., 2015). Pyridine causes stench, nerve toxicity, and 53 serious damage to the cornea (Li et al., 2014). With the rapid 54development of the economy and chemical industry, pyridine 55has become a common organic pollutant which can cause 56

serious damage to human health. Because pyridine has high 57 volatility and solubility in water, pyridine wastewater is 58 produced during the process of production and application 59 of pyridine and its derivatives. This kind of wastewater is 60 highly concentrated and refractory to biodegradation. 61

According to the currently utilized technologies, pyridine 62 wastewater can be treated by coagulation, adsorption, chem- 63 ical oxidation, Fenton oxidation, photocatalytic oxidation, and 64 direct incineration methods (Bai et al., 2010; Tian et al., 2013). 65 However, coagulation and adsorption methods cannot re- 66 move the pyridine-class pollutants effectively. Although 67 chemical oxidation methods can remove COD, the degrada- Q4 tion efficiency for pyridine is too low, and these methods also 69 result in secondary pollution. Fenton oxidation may oxidize 70 recalcitrant pollutants and refractory organics in the chemical 71 oxidation process. Unfortunately, the Fenton reagent method 72

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serious damage to human health. Becau volatility and solubility in water, pyr hemical raw produced during the process of produc

A novel cathodic-anodic-electrolysis packing (CAEP) used in the treatment of pyridine

wastewater was researched, which mainly consisted of 4,4'-diamino-2,2'-disulfonic acid 15

(DSD acid) industrial iron sludge. The physical properties and morphology of the packing 16

were studied. The CAEP was used in a column reactor during the pretreatment of pyridine 17

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#### wastewater. The influence of pH, hydraulic retention time (HRT), the air–liquid ratio (A/L) 18 and the initial concentration of pyridine were investigated by measuring the removal of 19 total organic carbon (TOC) and pyridine. The characterization results showed that the bulk 20 density, grain density, porosity and specific surface area were 921 kg/m<sup>3</sup>, 1086 kg/m<sup>3</sup>, 43%, <sup>29</sup> and 29.89 m<sup>2</sup>/g, respectively; the removal of TOC and pyridine could reach 50% and 58% at <sup>30</sup> the optimal experimental conditions (pH = 3, HRT = 8 hr, A/L = 2). Notably, the surface of <sup>31</sup> the packing was renewed constantly during the running of the filter, and the handling <sup>32</sup>

capacity was stable after running for three months.

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has some shortcomings, such as high-cost reagents, complex 73 processes, large amounts of waste residues, and inevitable 74 secondary pollution. Photocatalytic oxidation processes have 75 been widely developed as a new research field in the past 76 decade. However, the related research is still in the experi-77 mental stage, and few photocatalytic oxidation processes 78 79 have been applied in practical industrial operations (Qiao and Wang, 2010). Accordingly, the most important purpose of the 80 81 current study is to find an effective method to solve the 82 problem of pyridine wastewater treatment. This research offers new approach using micro-electrolysis technology for 83 the pretreatment of pyridine wastewater. 84

Micro-electrolysis technology, also referred to as internal 85 electrolysis, is a kind of novel reaction based upon an electro 86 chemical mechanism, which was acknowledged in China in 87 1980s (Liu et al., 2012; Ning et al., 2015). It is based on the 88 primary battery between Fe<sup>0</sup> and carbon (C). During the 89 reaction of the primary battery, Fe<sup>0</sup> acts as the anode, losing 90 electrons, and C as the cathode, where H<sup>+</sup> gains electrons. The 91 working mechanism of micro-electrolysis technology is the 92following: (1) the reduction of Fe<sup>0</sup> and evolution of new [H<sup>0</sup>]; 93 (2) the flocculation of  $Fe(OH)_x$  produced by the reaction; 94 (3) the sedimentation of cathodic-anodic-electrolysis products; 95 96 (4) adsorption by the packing.

According to recent research, micro-electrolysis technology 97 98 has been chosen by more and more industries in the water 99 treatment process, such as for electroplating wastewater, 100 petrochemical industry wastewater, printing and dyeing wastewater, and other industry wastewater that is hard to degrade. 101 The structure of many organic pollutants can be degraded 102during the micro-electrolysis treatment process, while some 103 biological methods are not able to accomplish this. This 104 treatment could increase the ratio of  $BOD_5$  to  $COD_{Cr}$  (B/C) in 105wastewater, which is helpful for subsequent biological treat-106 ment, enabling treated wastewater to reach the national 107 discharge standard (Li et al., 2008; Luo et al., 2014; Ying et al., 108 2012b; Zhang et al., 2015). In the conventional micro-electrolysis 109reaction, the contact area between the wastewater and the 110 packing could be decreased during operation due to hardening 111 of the packing during the working process, which reduces the 112 treatment efficiency toward contaminants. What's more, this 113 hardening also suspends the micro-electrolysis reaction (Lai 114 et al., 2013; Ruan et al., 2010; Ying et al., 2012a; Zhang et al., 1152014). As a consequence, development of a novel kind of 116unhardened cathodic-anodic-electrolysis packing is urgently 117 needed (Wang et al., 2013). 118

Iron sludge produced during chemical production process-119es is a hazardous waste. There are many kinds of iron sludge, 120and 4,4'-diamino-2,2'-disulfonic acid (DSD acid) iron sludge is 121 one of them. According to the requirements for the treatment 122of hazardous waste, the iron sludge must be transported to a 123 hazardous waste disposal center to be safely solidified and 124 landfilled. In recent years, some research on the treatment 125and re-use of iron sludge has been carried out. One idea has 126127 been to recover the iron content for iron-making. Even though this method is cheap, there are often many organics in iron 128sludge that can impact the quality of iron. In another 129development, iron sludge was used as the raw material of 130 pigment. However, the related production process is very 131 complex. In addition, some researchers have used iron sludge 132

to produce inorganic salts and nanomaterials, which is not 133 efficient. Even though these studies provide some ideas for 134 the treatment of the iron sludge, the processes would be 135 difficult to achieve during actual production. Most of this 136 research involves Fenton iron sludge. DSD acid industrial iron 137 sludge is generated during the production process of DSD 138 acid. The DSD acid industrial iron sludge is rich in iron 139 because the iron serves as a catalyst during the production 140 process of DSD acid. What's more, the DSD acid industrial iron 141 sludge also contains many organics. Therefore, the DSD acid 142 industrial iron sludge is not only a hazardous waste but also a 143 potential resource. Research on the treatment of DSD acid 144 industrial iron sludge has been rare.

The current study used the iron and organics in DSD acid 146 industrial sludge to produce micro-electrolysis packing. The 147 iron and organics were transformed into Fe<sup>0</sup> and C by 148 pyrolysis, the Fe<sup>0</sup> and C served as the raw materials for the 149 micro-electrolysis packing. Then the packing was used to 150 treat refractory organic wastewater, which not only achieved 151 reuse of the DSD acid industrial sludge and realized resource 152 recovery, but also accomplished the aim of treating waste 153 with waste. In recent years, many granular packing materials 154 consisting of sewage sludge and solid pollutants have been 155 studied: for example, using novel ceramic particles consisting 156 of sludge and fly ash in the treatment of synthetic wastewater 157 (including glucose, soluble starch, sodium acetate trihydrate, 158 ammonium sulfate, peptone, potassium biphosphate) (Han 159 et al., 2009); utilizing ultra-lightweight ceramics fabricated from 160 sewage and clay (Qi et al., 2010); using ceramic-corrosion-cell 161 fillers made from clay and sewage sludge in the treatment of 162 cyclohexanone industry wastewater (Wu et al., 2011); and using 163 micro-electrolysis ceramic packing that consisted of clay, scrap 164 iron, and powdered activated carbon in the treatment of 165 acrylonitrile wastewater (Huang et al., 2016). In the current 166 study, a novel kind of cathodic-anodic-electrolysis packing 167 made from DSD acid industrial iron sludge and clay was 168 produced using pyrolysis technology. 169

This novel packing has improved adsorption ability be- 170 cause of its porosity. On the other hand, this packing is good 171 at avoiding the problem of hardening in the operation of the 172 cathodic-anodic-electrolysis process due to the renewal of the 173 surface during use. Importantly, all of materials utilized are 174 waste products. Additionally, the use of DSD acid industrial 175 iron sludge technology could reduce the amount of iron 176 powder needed due to its high iron content, making it much 177 cheaper than other materials. A simple and easy operation 178 process with low secondary pollution could be obtained by 179 using a column reactor (Chen et al., 2011; Huang et al., 2013). 180 This method not only achieved the recycling of clay and 181 industrial iron sludge, but also provided a novel method and 182 material for the pretreatment of pyridine wastewater. The 183 crucial factor in the production process of this packing is 184 maintaining the proper intensity. In this case the iron can be 185 consumed during the process of treatment of wastewater, 186 which destroys the structure of the surface of packing; as a 187 consequence, the surface layer of the packing is shed and the 188 surface of packing is continuously renewed. This characteris- 189 tic can delay the hardening of the packing and improve the 190 back-washing process effectively. Thus, the problem of 191 hardening and channeling was solved and the effectiveness 192

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