

Characterization of an innovative device controlling gaseous exchange in packages for food products

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ABSTRACT

The work describes both the characterization carried out and the experimental results from an innovative device allowing the gas exchange across a sealed package. The device is especially suitable for fresh fruit and vegetable preservation during cold storage, as it allows for the management of the headspace atmosphere inside sealed packages containing food products presenting metabolic activity.

Characterization results confirm the device's suitability for managing the bidirectional gas flow. For each tested device, the hydro-dynamical parameter and the diffusion parameter have been measured to define its steady-state behaviour. The steady-state gas concentrations reached in the package show the aptness of the devices for use with specific products; these equilibrium gas concentrations depend on the device type and on the mass of product contained in the package.

The results of simulated storage demonstrate that some products (pomegranate arils and table grapes) require preconditioning of the package free volume to reach the optimal gas concentrations in a short time. Other products (black truffle) with very high metabolic activity could reach the optimal condition without package preconditioning depending on the free volume.

1. Introduction

Packaging methods and surrounding atmosphere composition are crucial for maintaining the organoleptic and nutritional characteristics of a product over time and to extend its shelf-life (Kalia and Parshad, 2015). Market demand for organic and pesticide/sulphite-free products creates increasing interest in treatments based on modified atmosphere shock treatment and/or packaging using low levels of oxygen and other gases having an effect on the metabolic activity of vegetable tissue or pathogens. Consequently, the food market requires continuous product innovation in packaging, thus creating a growing demand for new technological solutions (Dainelli et al., 2008).

Until now, the approach has been the development of polymeric films to achieve improvements in the organoleptic and microbial quality of the fruits and vegetables treated, as it is well known that, for proper preservation of foodstuffs, it is necessary to maintain the correct gas composition within the package, and that this objective can be achieved using the correct packaging materials.

Modified atmosphere packaging (MAP) technology gives the advantage of packaging perishable products after harvest allowing for extension of their shelf-life, thereby restraining distribution costs with

minimal effect on the nutritional value or organoleptic quality of the product (Mastromatteo et al., 2010).

MAP technology basically consists of the substitution of the surrounding atmosphere of a packaged product with a modified atmosphere. The gases mainly used in MAP are CO₂, N₂ and/or O₂ (Rutherford et al., 2007). In addition, MAP, in combination with low-temperature storage, is an effective tool to prolong shelf-life of food products because, generally, low O₂ or high CO₂ concentrations decrease produce respiration, postharvest pathogens and the rate of deterioration (Kader et al., 1989). Therefore, product deterioration processes are slowed down, respiration decreases and shelf-life is prolonged.

However, to prevent anaerobic conditions as a result of oxygen consumption, it is necessary to use permeable materials so that oxygen can freely flow from external air into the package. The choice of packaging material is related to the required barrier effect against gases and water vapour, depending on the desired residual amount of each gas to be exchanged over time with the outside environment at steady-state (Agar et al., 1999). Therefore, the packaging material is very important, and it represents a strategic choice as it affects the final characteristics of the product and a significant part of production costs

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Nomenclature

Indices in vector and subscripts

1	is O ₂	L-MMAD	Long type device
2	is CO ₂	M _i	Molar mass of gas “i” (kg mol ⁻¹)
3	is N ₂	M _m	Molar mass of gas mixture (kg mol ⁻¹)
μ	Gas viscosity (Pa s)	MAP	Modified atmosphere packaging
ΔC	Vector of ΔC _i	mc	Model coefficient of CO ₂ respiration rate eq. (3)
ΔC _i	C _{i,out} -C _i , differential molar concentration of gas “i” across the device (mol m ⁻³)	mo	Model coefficient of O ₂ respiration rate eq. (2)
ΔP _p	P _{out} -P _p , differential pressure across the device (Pa)	MMAD	Micro-machined adhesive device
ΔP _i	P _{i,out} -P _i , differential pressure of gas “i” across the device	N	Vector of N _i
ΔP _{p0}	P _{out} -P _{p0} , differential pressure across the device (Pa) at time t = 0	N _i	Moles of gas “i” in package (mol)
ΣV _i	“diffusion volume” of gas “i” (Fuller et al., 1966)	N _p	Overall moles of gas in the package (mol)
ΣV _m	“diffusion volume” of the gas mixture (Fuller et al., 1966)	N _i ^F	Vector of N _i ^F
ac	Model coefficient of CO ₂ respiration rate eq. (3)	N _i ^F	Moles of gas “i” in the package (mol) due to diffusion and hydro-dynamical mechanism
ao	Model coefficient of O ₂ respiration rate eq. (2)	nc	Model coefficient of CO ₂ respiration rate eq. (3)
A	Device active cross-sectional area (m ²)	no	Model coefficient of O ₂ respiration rate eq. (2)
C _i	N _i /V, molar concentration of gas “i” in the package (mol m ⁻³)	P _i	Partial pressure of gas “i” in the package (Pa)
C _{i,out}	Molar concentration of gas “i” external to the package (mol m ⁻³)	P _p	Pressure in the package (Pa)
C _{out}	Molar concentration of gas mixture external to the package (mol m ⁻³)	P _{p0}	Pressure in the package (Pa) at time t = 0
C _x	Vector of C _{i,x}	P _{i,0}	Partial pressure of gas “i” in the package (Pa) at time t = 0
C _{i,x}	= C _i if ΔP _p < 0, = C _{i,out} if ΔP _p ≥ 0 (mol m ⁻³)	P _{i,out}	Partial pressure of gas “i” external to the package (Pa)
C _p	N _p /V, molar concentration of gas mixture in the package (mol m ⁻³)	P _{i,x}	= P _i if ΔP _p < 0, = P _{i,out} if ΔP _p ≥ 0
d	Device active cross-sectional area diameter (m)	P _{out}	Pressure external to the package (Pa)
D _{ij}	Diffusivity coefficient of gas “i” into gas “j” (m ² s ⁻¹)	RR _{O₂}	Respiration rate expressed as consumption of O ₂ (mol kg ⁻¹ s ⁻¹)
D _{im}	Diffusivity coefficient of gas “i” into gas mixture (m ² s ⁻¹)	RR _{CO₂}	Respiration rate expressed as production of CO ₂ (mol kg ⁻¹ s ⁻¹)
dc	Model coefficient of CO ₂ respiration rate eq. (3)	RR	Vector of respiration rates RR _i
do	Model coefficient of O ₂ respiration rate eq. (2)	RR _i	Component related to gas “i” of vector of respiration rates (mol kg ⁻¹ s ⁻¹)
F _{im}	Diffusion parameter of the device with regard to gas “i” (m ³ s ⁻¹)	RQ	Respiratory quotient (RR _{CO₂} /RR _{O₂})
G	Mass matrix of the differential equations set	PO ₂	Partial pressure of O ₂ (Pa)
H	Hydro-dynamic parameter of the device (m ³ Pa ⁻¹ s ⁻¹)	PCO ₂	Partial pressure of CO ₂ (Pa)
HPVR	Headspace to product volume ratio	R	Gas constant (8.314 J mol ⁻¹ K ⁻¹)
J	Vector of J _i	S-MMAD	Short type device
J _i	Molar flow of gas “i” (mol m ⁻² s ⁻¹)	STP	Standard temperature and pressure (0 °C and 10 ⁵ Pa)
J _i ^F	Molar flow of gas “i” (mol m ⁻² s ⁻¹) due to diffusion and hydro-dynamical mechanism	T	Constant temperature (K)
J ^F	Vector of J _i ^F	V	Constant container volume (m ³)
kc	Model coefficient of CO ₂ respiration rate eq. (3)	Vo	Measuring apparatus internal volume (m ³)
ko	Model coefficient of O ₂ respiration rate eq. (2)	zc	Model coefficient of CO ₂ respiration rate eq. (3)
L	Device active length (m)	zo	Model coefficient of O ₂ respiration rate eq. (2)
		w	Mass of product in the container (kg)
		X _i	N _i /N _p = P _i /P _p , molar fraction of gas “i” in the package
		X _{i,out}	P _{i,out} /P _{out} , molar fraction of gas “i” external to the package
		X _{i,x}	= X _i if ΔP _p < 0, = X _{i,out} if ΔP _p ≥ 0
		X _{i,out}	P _{i,out} /P _{out} , molar fraction of gas “i” external to the package
		XO ₂	Molar fraction of O ₂
		XCO ₂	Molar fraction of CO ₂

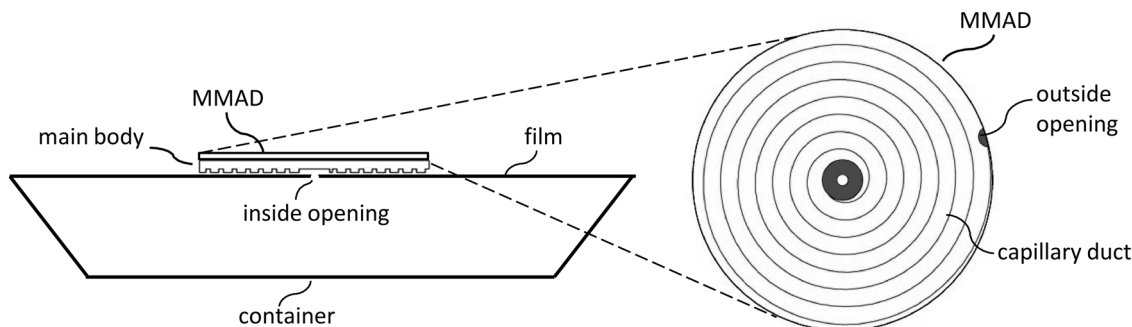


Fig. 1. Working principle of the MMAD and its application to a container.

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