

# Photocatalytic decolorization of methyl orange in aqueous medium of $\text{TiO}_2$ and $\text{Ag-TiO}_2$ immobilized on $\gamma\text{-Al}_2\text{O}_3$

Lung-Chuan Chen\*, Fu-Ren Tsai, Chao-Ming Huang

*Department of Environmental Engineering, Kun-Shan University of Technology, Yung Kang City, Tainan 710, Taiwan, ROC*

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## Abstract

$\text{TiO}_2$ , synthesized through a sol–gel procedure with acetylacetone chelating agent, was immobilized on  $\gamma\text{-Al}_2\text{O}_3$  and deposited with photoreduced Ag. The prepared catalysts were characterized and applied for decolorization of methyl orange (MO). The photoactivity of  $\text{TiO}_2/\gamma\text{-Al}_2\text{O}_3$  is affected by the  $\text{H}_2\text{O}/\text{Ti}$  molar ratio applied in the sol–gel process. The optimal calcination temperatures of the  $\text{TiO}_2/\gamma\text{-Al}_2\text{O}_3$  locate in the ranges from 723 to 773 K and 773 to 873 K as  $\text{TiO}_2$  prepared with  $\text{H}_2\text{O}/\text{Ti}$  of 10 and 1, respectively. Incorporating photoreduced Ag to  $\text{TiO}_2/\gamma\text{-Al}_2\text{O}_3$  leads to reduction reaction of methyl orange in addition to oxidation reaction, and yields a significant increment in decolorization efficiency. The optimal Ag load on  $\text{TiO}_2/\gamma\text{-Al}_2\text{O}_3$  and dosage of  $\text{Ag}/\text{TiO}_2/\gamma\text{-Al}_2\text{O}_3$  in the photodecolorization of methyl orange are about 1.0% and 1.0 g/L, respectively. The photocatalytic rate is proportional to the Ag load and catalyst dosage raised to the powers of 0.45 and 0.71, respectively.

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## 1. Introduction

Recently, photocatalytic processes have been receiving much attention, particularly for the complete destruction or mineralization of the toxic and non-biodegradable compounds to carbon dioxide and inorganic constituents in both water and gas phases [1–4]. Among the photocatalysts applied, titanium dioxide is the most popular one due to the peculiarities of chemical inertness, suitable bandgap energy, non-photocorrosion and non-toxic influence on the microorganisms, etc. Owing to the policies of efficient utilization of solar energy, high quantum efficiency and convenience of operation, the present researches of the photocatalytic processes have focused on the designs and constructions of new light energy sources, photochemical reactors, preparations of novel photocatalysts and their supports [1].

Irradiation of  $\text{TiO}_2$  semiconductor by light with energy equal to or greater than its bandgap energy leads to exci-

tation of an electron from the valence band to the conduction band. Charge separation is then formed. The electrons in the conduction band behave as a cathode and promote the reduction reactions of oxidized compounds with potentials positive to that of the lowest conduction band. On the other hand, positive holes ( $h^+$ ) are generated in the valence band. The holes show high affinities for electrons and behave as an anode to oxidize the reduced compounds with potentials negative to that of the highest valence band or to oxidize the adsorbed  $\text{H}_2\text{O}$  or  $\text{OH}^-$  to hydroxyl radical ( $\text{HO}^\bullet$ ). Hydroxyl radicals are very reactive neutral species, which react rapidly and non-selectively with the contaminants preadsorbed on titanium dioxide surface. Accordingly,  $\text{HO}^\bullet$  is the chief oxidant for photocatalytic degradation in wastewater treatment [2,5].

In the past few years, titanium dioxide-suspended systems were widely applied for the photocatalytic processes. It revealed a fair photoactivity, but the separation of the finely powdered titanium dioxide from the slurry system was very difficult. Hence, the immobilization of  $\text{TiO}_2$  on supports to improve the separated efficiency has attracted much attention.

\* Corresponding author. Tel.: +886 6 2050137; fax: +886 6 2050540.

E-mail address: [lcchen@mail.ksut.edu.tw](mailto:lcchen@mail.ksut.edu.tw) (L.-C. Chen).

However, the immobilization usually decreases the overall photoactivity of  $\text{TiO}_2$  [1,6–8]. Also, the blue shift of the absorption band occurs with immobilization, and then decreases the utilization of solar energy [9,10]. Recently, binary metal oxides systems, such as  $\text{TiO}_2/\text{SiO}_2$  [11–15], were investigated to enhance photoactivity. An analysis of these systems reveals that large surface area and preferential adsorption of the reacted molecules on  $\text{SiO}_2$  will promote the photoactivity [12]. Additionally, Fu et al. [11] indicated that the surface acidity of  $\text{TiO}_2$  increased with addition of  $\text{SiO}_2$ . These surface acidic sites were said to be in the form of stronger surface hydroxyl groups, which accepted holes generated by illumination and sequentially oxidized the adsorbed molecules and prevented recombination of electrons and holes. Therefore, the photoactivity increases, however, it needs to be further improved for commercial application.

Aluminum oxide, with high surface area and acidity, is widely used as catalyst's support. Kato [16] also pointed out that  $\gamma\text{-Al}_2\text{O}_3$  was not harmful to the photocatalytic activity of  $\text{TiO}_2$ . Furthermore, introduction of platinum or silver to the titanium dioxide photocatalytic system can increase the photocatalytic efficiency [2,17–21]. Unfortunately, few reports concerned about the immobilization of  $\text{TiO}_2$  on  $\gamma\text{-Al}_2\text{O}_3$  with deposited metal [13,21]. Accordingly,  $\text{TiO}_2/\gamma\text{-Al}_2\text{O}_3$  photocatalysts with and without photodeposited Ag are prepared and characterized by X-ray diffraction (XRD), UV-diffusion reflectance spectroscopy and FTIR. Finally, methyl orange is used as a probe for the photocatalytic decolorization due to the relatively high toxicity and complex structure, which both make it difficult to be treated by microorganisms.

## 2. Experimental

$\gamma\text{-Al}_2\text{O}_3$  (Merck) with a surface area and a pore volume of  $162\text{ m}^2/\text{g}$  and  $0.45\text{ cm}^3/\text{g}$ , respectively, was used as carrier. The particle size of the  $\gamma\text{-Al}_2\text{O}_3$  was sieved to be in the range from 200 to 270 mesh. Titanium isopropoxide (TTIP; TCI, EP), acetylacetone (ACAC; Lancaster, EP), ethanol (Scharlance, 99.8%), HCl (Ferak, GR) and silver nitrate (Katayama Chem. Co., special grade) were all used as received. Methyl orange (MO; Merck) was dissolved in ultra pure water (Milli Pore  $\text{Q}^+$ ) to a desired concentration. The pH of the solution was adjusted to the desired value by NaOH or HCl and measured by a pH meter (Suntex, SP-701). The prepared MO solution was stored in the dark and used within a week.

A 0.5 M solution of TTIP in ethanol was prepared; subsequently, ACAC was added to result a clear-yellow solution. A molar ratio of  $\text{ACAC}/\text{TTIP} = 1$  was used. The solution was stirred at room temperature for 3 h.  $\text{H}_2\text{O}$  of pH 1.5 or 7.0, adjusted by HCl and NaOH, was added drop by drop to the solution under vigorous stirring, and the prepared  $\text{TiO}_2$  were designed as A- and N-types corresponding to the acidic and neutral media, respectively. The molar ratio of  $\text{H}_2\text{O}/\text{TTIP}$  was a studied factor and changed from 1 to 20. This sol was stirred at room temperature for 3 h, after which  $\gamma\text{-Al}_2\text{O}_3$  powder was

added slowly with vigorous stirring. The final solution was kept on stirring at 323 K for 24 h. The solid samples were filtered, washed by water and dried in air at 373 K for 24 h, eventually calcinated at the desired temperature for 3 h. Then, the  $\text{TiO}_2/\gamma\text{-Al}_2\text{O}_3$  proceeded photoreduction [22] with silver nitration to make  $\text{Ag}/\text{TiO}_2/\gamma\text{-Al}_2\text{O}_3$  photocatalysts by an UV light source (Philip, HPI-T400 W).

The bonding structures of the prepared photocatalysts were analyzed by FTIR (Jasco, FTIR-410 with DR-81). XRD (Rigaku D/Max III.V) technique and UV-diffusion reflection spectroscopy (Hitachi, U3010) were applied to study the crystal type and absorption bandgap energy. The surface area and pore volume were determined by BET method (Micromeritics, ASAP2400).

The photoactivity test was conducted in a Pyrex glass reactor of about 80 mm in diameter and 100 mm in height. The reactor was provided with a water jacket to control the reaction temperature. The cover of the reactor had ports for sampling, a thermal meter, a gas disperser and a condenser. A 400 W medium pressure mercury lamp (Philip, HPI-T400 W) was used as the light source. A magnetic stirrer operated at 600 rpm was used to provide a good mixing.

At the beginning of a run, 300 mL MO solution was fed to the reactor, and then it was kept at 303 K. The desired amount of the photocatalyst was added, and oxygen or nitrogen was bubbled through the gas disperser into the reactor at 250 mL/min. After 2 h premixing, to attain the adsorption equilibrium of MO on the photocatalyst, the run was started by illuminating the light source. Samples were periodically taken from the reactor and analyzed by an UV–vis spectrophotometer (Perkin-Elmer,  $\lambda 2$ ).

## 3. Results and discussion

### 3.1. Characteristics of the prepared $\text{TiO}_2/\gamma\text{-Al}_2\text{O}_3$ photocatalysts

Fig. 1 depicts the XRD profiles of the pure  $\gamma\text{-Al}_2\text{O}_3$  carrier and  $\text{Ag}/\text{TiO}_2/\gamma\text{-Al}_2\text{O}_3$  photocatalysts. It appears that the  $\text{TiO}_2$  is amorphous after calcination at 473 K, and  $\gamma\text{-Al}_2\text{O}_3$  surface is almost covered by  $\text{TiO}_2$ , since the peaks near  $38^\circ$  and  $46^\circ$  belong to  $\gamma\text{-Al}_2\text{O}_3$  and are severely suppressed. Increasing calcination temperature to 673 K transfers  $\text{TiO}_2/\gamma\text{-Al}_2\text{O}_3$  to the anatase phase. Further increasing the calcination temperature to 973 K yields the rutile phase in addition to the anatase phase. The fraction of rutile phase increases with decreasing  $\text{H}_2\text{O}/\text{Ti}$  applied in the sol–gel procedure. Incorporation of Ag to  $\text{TiO}_2/\gamma\text{-Al}_2\text{O}_3$  cannot alter the XRD patterns and reveals no Ag diffraction peak, which may be ascribed to little content. The crystal size of  $\text{TiO}_2/\gamma\text{-Al}_2\text{O}_3$  increases from 15.7 to 25.2, 10.5 to 20.1 and 8.5 to 17.7 nm as the calcination temperature increases from 673 to 973 K with  $\text{H}_2\text{O}/\text{Ti}$  of 1, 10 and 20, respectively, as shown in Fig. 2. With lower  $\text{H}_2\text{O}/\text{Ti}$  ratio, TTIP is not completely hydrolyzed and leads to larger crystal size. Also, increasing calcination

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